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(54) **Title:** ANTIMICROBIAL **VACCINE COMPOSITIONS** 

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**IS7) Abstract:** This invention is directed to antimicrobial vaccine compounds and compositions comprising oligosaccharide  $\beta$ -(1--6)-**5** glucosamine groups having from **3** to 12 glucosamine units linked through a linker group to tetanus toxoid wherein the toxoid is primarily in its monomeric form This invention is also directed to vaccine compositions that provide natural immunity against microbes possessing a cell wall structure tha comprises oligosaccharide N-acetyl-β-(1->6)-glucosamine (PNAG) structures.

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# *ANTIMICROBIAL VACCINE COMPOSITIONS*

### *Cross-Reference to Related Application*

**[0001]** This application claims priority to **U.S.** provisional application no. **62/892,400,**  filed on August **27, 2019,** which is incorporated herein **by** reference in its entirety.

## *Field of the Invention*

**[0002]** This invention is directed to antimicrobial vaccine compounds and compositions comprising oligosaccharide  $\beta$ - $(1\rightarrow6)$ -glucosamine groups having from 3 to 12 glucosamine units linked through a linker group to tetanus toxoid wherein the toxoid is primarily in its monomeric form. This invention is also directed to vaccine compositions that provide natural immunity against microbes possessing a cell wall structure that comprises oligosaccharide N-acetyl-f-(1->6)-glucosamine **(PNAG)** structures.

# *State of the Art*

**[0003]** Oligosaccharide antigens attached to a toxoid carrier are known to produce a weak immune response especially in children and the elderly. When oligosaccharides are conjugated to a toxoid carrier to form a vaccine, it is desirable to attach or load as many oligosaccharide groups onto the carrier to enhance the overall immune response generated. In general, a vaccine containing more oligosaccharide antigens loaded onto a carrier will generate a higher antibody titer than a similar vaccine containing fewer oligosaccharide antigens.

**[0004]** Vaccines that employ tetanus toxoid as the carrier with multiple copies of the oligosaccharide bound thereto are known in the art. Conventionally, attachment of oligosaccharide groups to the toxoid is through a linker that couples to reactive amino groups (e.g., **-NH2** as found on lysine residues) on the toxoid. Although the chemistry is well established, there are a number of complications in dealing with toxoid chemistry.

**[0005]** First, tetanus toxoid is prepared **by** treating tetanus toxin with a chemical such as formaldehyde that renders it non-toxic when administered but still antigenic. Formaldehyde reacts with reactive amino groups on the toxin thereby reducing the number of remaining reactive amino groups on the toxoid that are useful for oligosaccharide coupling. Moreover, the number of reactive amino groups on the treated toxoid will vary

from manufacturer to manufacturer. Second, the manufacturing process for tetanus toxoid also results in low molecular weight contamination in the tetanus toxoid composition. These contaminants include low molecular weight reactive amino functionalities that compete with the toxoid for oligosaccharide coupling.

**[0006]** The art has previously disclosed antimicrobial vaccines comprising penta- $\beta$ - $(1\rightarrow 6)$ -glucosamine groups linked to the tetanus toxoid where the loading factor for attachment of these penta- $\beta$ -(1 $\rightarrow$ 6)-glucosamine groups ranges from as low as 12 and up to 20 **-** Gening, et al., Infect. Immun., **78(2):764-772** (2010). However, this loading factor is less than desirable and apparently is based on underlying synthetic problems associated with the toxoid and coupling chemistry.

**[0007]** Accordingly, it would be desirable to provide for a higher level of loading onto tetanus toxoid.

#### *SUMMARY OF THE INVENTION*

**[0008]** This invention is directed to the discovery that vaccine compounds with loading levels of at least 25 and preferably from about 31 to 39 oligomeric  $\beta$ - $(1\rightarrow 6)$ -glucosaminelinked groups onto tetanus toxoid having from at least 25 and preferably **31** reactive amino functionalities can be achieved provided that the toxoid component in the vaccine compounds comprises at least **85** percent of the toxoid in monomeric form. In one embodiment, the toxoid component in the vaccine compounds comprises at least **90**  percent of the toxoid in monomeric form, or any subvalue or subrange there between. In some embodiments, the toxoid includes at least **90** percent to the **99.9** percent of the toxoid in monomeric form and preferably at least **95** percent to **99.9** percent of the toxoid in monomeric form, or any subvalue or subrange there between. In one embodiment, the amount of low molecular weight reactive amino compounds is no more than **3** weight percent relative to the weight of toxoid present. In another embodiment, the amount of low molecular weight amino compounds in the composition is less than 2 weight percent and preferably less than **1** weight percent based on the weight of the toxoid present and even more preferably less than **0.5** weight percent based on the weight of the toxoid present. In another preferred embodiment, the amount of monomer is over **99** area percent, for example, based on HPLC.

**[0009]** Accordingly, in one embodiment, this invention provides for a vaccine composition that comprises at least 25 and preferably from about **31** to about **39**  oligomeric- $\beta$ -(1 $\rightarrow$ 6)-glucosamine groups linked units onto a tetanus toxoid carrier via a linker wherein the oligomer comprises from 3 to 12 repeating  $\beta$ - $(1\rightarrow6)$ -glucosamine units provided that less than about 40 number percent of the total number of such units are **<sup>N</sup>** acetylated and further wherein said tetanus toxoid comprises at least 25 and preferably at least **31** reactive amino functionalities and at least **85** percent of the toxoid components are in monomeric form, or in some embodiments, at least **90%.** Such vaccine compositions provide effective immunity to a patient against microbial infections wherein said microbe comprises oligomeric N-acetyl- $\beta$ -(1 $\rightarrow$ 6)-glucosamine structures in its cell walls.

**[0010]** In one embodiment, this invention provides for a compound represented **by**  formula I:

 $(A-B)_x-C$  **I** 

where A comprises from 3 to 12 repeating  $\beta$ - $(1\rightarrow 6)$ -glucosamine units or mixtures thereof having the formula:



B is of the formula:



where the left side of the formula is attached to **C** and the right side is attached to **A;**  and **C** is tetanus toxoid having at least **31** reactive amino functionalities;

*x* is an integer from about **31** to about **39;** 

*y* is an integer from **1** to **10;** and

R is hydrogen or acetyl provided that no more than 40% of the R groups are acetyl

wherein said tetanus toxoid comprises at least **31** reactive amino groups and at least **90**  percent **by** number of the toxoid is in monomeric form.

**[0011]** In one embodiment, this invention provides for a vaccine composition that is useful against microbes which comprise oligomeric N-acetyl- $\beta$ - $(1\rightarrow6)$ -glucosamine structures in their cell wall wherein said vaccine composition comprises a pharmaceutically acceptable carrier and an effective amount of a vaccine represented **by** formula I:

$$
(A-B)_{x} - C \qquad I
$$

where A comprises from 3 to 12 repeating  $\beta$ - $(1\rightarrow 6)$ -glucosamine units or mixtures thereof having the formula:



B is of the formula:



where the left side of the formula is attached to **C** and the right side is attached to **A;**  and **C** is tetanus toxoid having at least **31** reactive amino functionalities; *x* is an integer from about **31** to about **39;** 

*y* is an integer from **1** to **10;** and

R is hydrogen or acetyl provided that no more than 40% of the R groups are acetyl wherein said tetanus toxoid comprises at least **31** reactive amino groups and at least **90**  percent **by** number of the toxoid is in monomeric form. Such vaccine compositions provide effective immunity to a patient against microbial infections wherein said microbe comprises oligomeric N-acetyl- $\beta$ -(1 $\rightarrow$ 6)-glucosamine structures in its cell walls.

**[0012]** In one embodiment of formula **I** above, there is provided a compound of formula II:

#### $(A'-B)<sub>x</sub>-C$  II

**HO**  HO  $\sim$  $H_0$   $N_{\rm H_2}$   $\sim$   $\sim$   $\sim$   $\sim$ **H NH2** HH **HO 1**  $\bigwedge_{\mathsf{NH}_{\mathbb{Q}_p}}$ **NH<sub>2</sub>** HO NH<sub>2</sub>

where A' is a penta- $\beta$ -(1 $\rightarrow$ 6)-glucosamine (carbohydrate ligand) group of the formula:

and B, **C** and x are as defined above, provided that at least **85** percent **by** number of the toxoid is in monomeric form, or in some embodiments, at least **90%.** 

**[0013]** In one embodiment, this invention provides for a vaccine composition against microbes comprising oligomeric N-acetyl- $\beta$ - $(1\rightarrow 6)$ -glucosamine structures in their cell wall wherein said vaccine composition comprises a pharmaceutically acceptable carrier and an effective amount of a vaccine represented **by** formula II

$$
(A'-B)_x-C
$$

where A' has the formula



and B, **C** and x are as defined above, provided that at least **85** percent **by** number of the toxoid components are in monomeric form, or in some embodiments, at least **90%.** 

**[0014]** In one embodiment, this invention provides for a method for providing effective immunity to a patient from microbes comprising oligomeric N-acetyl- $\beta$ - $(1\rightarrow 6)$ -glucosamine groups in their cell wall which method comprises administering a compound of formula **I** or II above.

**[0015]** In one embodiment, this invention provides for a method for providing effective immunity to a patient from microbes comprising oligomeric N-acetyl- $\beta$ - $(1\rightarrow6)$ -glucosamine groups in their cell wall which method comprises administering a pharmaceutical composition of this invention as described above to said patient.

**[0016]** In one embodiment, the compounds of this invention include those where **x** is from **33** to **39.** In another embodiment, the compounds of this invention include those where x is from **35-38.** 

**[0017]** Representative compounds of this invention are set forth in the table below:





**[0018]** In one embodiment, the compositions of this invention comprise no more about **3** weight percent of low molecular weight amino groups based on the total weight of the compound of formula **I** or II.

**[0019]** In one embodiment, this invention provides methods for providing immunity to a patient against microbes comprising oligosaccharide  $\beta$ -(1 $\rightarrow$ 6)-glucosamine groups in their cell wall which methods comprise administering to said patient an effective amount of a compound represented **by** formula I:

$$
(A-B)_{x} - C \qquad I
$$

wherein **A,** B, **C** and x are as defined above and elsewhere herein.

**[0020]** In one embodiment, this invention provides methods for providing immunity to a patient against microbes comprising N-acetyl oligosaccharide  $\beta$ - $(1\rightarrow 6)$ -glucosamine groups in their cell wall comprising administering to said patient an effective amount of the compounds of formula **I** as defined above and elsewhere herein, in which **y** is 2, **3,** or 4 as well as mixtures thereof.

**[0021]** In one embodiment, this invention provides methods for providing immunity to a patient against microbes comprising N-acetyl oligosaccharide  $\beta$ - $(1\rightarrow 6)$ -glucosamine groups in their cell wall which methods comprise administering to said patient an effective amount of the compounds of formula II:

$$
(A'-B)_x-C \qquad II
$$

where A' is a penta- $\beta$ -(1 $\rightarrow$ 6)-glucosamine (carbohydrate ligand) group of the formula:



and B, **C** and x are as defined above and elsewhere herein.

[0022] In one embodiment, this invention provides methods for providing effective immunity to a subject against microbes comprising N-acetyl oligosaccharide  $\beta$ - $(1\rightarrow6)$ glucosamine groups in their cell wall which methods comprise administering to said patient an effective amount of the pharmaceutical composition of a pharmaceutically acceptable diluent and an effective amount of the compound of formula I:

$$
(A-B)_x-C-I
$$

wherein **A,** B, **C** and x are as defined above and elsewhere herein.

**[0023]** In one embodiment, this invention provides methods for providing effective immunity to a subject against microbes comprising N-acetyl oligosaccharide  $\beta$ - $(1\rightarrow6)$ glucosamine groups in their cell wall, which methods comprise administering to said patient an effective amount of the pharmaceutical composition of a pharmaceutically acceptable diluent and an effective amount of the compound of formula **I** as defined above and elsewhere herein, in which **y** is 2, **3,** or 4.

**[0024]** In one embodiment, this invention provides methods for providing effective immunity to a subject against microbes comprising N-acetyl oligosaccharide **p-(1->6)** glucosamine groups in their cell wall, which methods comprise administering to said patient an effective amount of the pharmaceutical composition of a pharmaceutically acceptable diluent and an effective amount of the compound of formula II:

$$
(A'-B)_x-C \qquad II
$$

where A' is a penta- $\beta$ -(1 $\rightarrow$ 6)-glucosamine (carbohydrate ligand) group of the formula:



and B, **C** and x are as defined above and elsewhere herein.

**[0025]** In one embodiment, this invention provides methods for providing effective immunity to a subject against microbes comprising N-acetyl oligosaccharide  $\beta$ - $(1\rightarrow6)$ glucosamine groups in their cell wall which methods comprise administering to said patient an effective amount of the above compounds as pharmaceutical compositions with a pharmaceutically acceptable diluent and an effective amount of the compound, wherein said patient has a white blood count of at least 2,000.

**[0026]** In some embodiments, in one or more of the aforementioned methods, the pharmaceutical compositions can include, for example, no more than about **3** weight percent of low molecular weight amino compounds, or in alternative embodiments, less than **1** weight percent of low molecular weight amino compounds, and any subvalue or subrange from **3** weight percent to zero.

#### *BRIEF DESCRIPTION OF THE DRAWINGS*

**[0027]** Figure **1** illustrates the 1H NMR for compound **17** (as described below).

**[0028]** Figure 2 illustrates the **<sup>1</sup> 3C** NMR for compound **17.** 

**[0029]** Figure **3** illustrates the HPLC spectrum for the separation of tetanus toxoid monomer from oligomers and low molecular weight amino compounds.

**[0030]** Figure 4 provides a HPLC trace of the conversion of the disulfide, compound **16,**  to two equivalents of the monosulfide, compounds **17.** 

#### *DETAILED DESCRIPTION OF THE INVENTION*

**[0031]** This invention provides for antimicrobial vaccine compounds and compositions wherein the compounds comprise at least 25 and preferably from **31** to **39** oligosaccharide f-(1->6)-glucosamine groups each having from **3** to 12 glucosamine units where each of said groups is linked to tetanus toxoid protein via a linker wherein no more than 40% of the individual glucosamine units possess an N-acetyl group and further wherein the tetanus toxoid comprises at least 25 and preferably at least **31** reactive amino groups and at least **85** percent, **90** percent, **95%** and **99% by** number of the toxoid components are in monomeric form, or any subvalue or subrange within **85%-99%.** 

**[0032]** The vaccine compositions described herein provide effective immunity to a patient against microbial infections wherein said microbe comprises oligomeric N-acetyl-ß- $(1\rightarrow 6)$ -glucosamine structures in its cell walls.

**[0033]** Prior to describing this invention in more detail, the following terms will first be defined. **If** a term used herein is not defined, it has its generally accepted scientific or medical meaning.

**[0034]** The terminology used herein is for the purpose of describing particular embodiments only and is not intended to be limiting of the invention. As used herein, the singular forms "a", "an" and "the" are intended to include the plural forms as well, unless the context clearly indicates otherwise.

**[0035]** "Optional" or "optionally" means that the subsequently described event or circumstance can or cannot occur, and that the description includes instances where the event or circumstance occurs and instances where it does not.

**[0036]** The term "about" when used before a numerical designation, e.g., temperature, time, amount, concentration, and such other, including a range, indicates approximations which may vary **by (+ )** or **( - ) 10%, 5%, 1%,** or any subrange or subvalue there between. Preferably, the term "about" when used with regard to a dose amount means that the dose may vary **by +/- 10%.** 

**[0037]** "Comprising" or "comprises" is intended to mean that the compositions and methods include the recited elements, but not excluding others. "Consisting essentially of' when used to define compositions and methods, shall mean excluding other elements of any essential significance to the combination for the stated purpose. Thus, a composition consisting essentially of the elements as defined herein would not exclude other materials or steps that do not materially affect the basic and novel characteristic(s) of the claimed invention. "Consisting of" shall mean excluding more than trace elements of other ingredients and substantial method steps. Embodiments defined **by** each of these transition terms are within the scope of this invention.

**[0038]** The term " $\beta$ -(1 $\rightarrow$ 6)-glucosamine unit" or "glucosamine unit" refers to individual glucosamine structures as follows:



where the 6-hydroxyl group is condensed with the **1** hydroxyl group of the preceding glucosamine unit and where the dashed lines represent binding sites to the preceding and succeeding glucosamine units. When combined with another " $\beta$ - $(1\rightarrow 6)$ -glucosamine unit, the resulting disaccharide has the structure:



**[0039]** The term " $\beta$ -(1 $\rightarrow$ 6)-glucosamine unit possessing an N-acetyl group refers to the structure:



where the 6-hydroxyl group of a second unit is condensed with the 1-hydroxyl group of the proceeding glucosamine unit.

**[0040]** The term "oligosaccharide comprising a " $\beta$ - $(1\rightarrow6)$ -glucosamine group" refers to that group on the compound that mimics a portion of the cell wall of pathogenic bacteria which are defined to be "oligosaccharide  $\beta$ - $(1\rightarrow6)$ -glucosamine structures" (as defined below). Again, such groups are limited to **3** to 12 p-(1->6)-glucosamine units wherein up to 40% of said units can possess a N-acetyl group. In one embodiment, less than **30%** of said  $\beta$ -(1 $\rightarrow$ 6)-glucosamine units are N-acetylated. In another embodiment, less than 20% of said  $\beta$ -(1 $\rightarrow$ 6)-glucosamine units are N-acetylated. Still, in another embodiment, less than 10% of said β-(1 $\rightarrow$ 6)-glucosamine units are N-acetylated. Yet still, in another embodiment, none of said  $\beta$ -(1 $\rightarrow$ 6)-glucosamine units are N-acetylated.

**[0041]** The term "oligosaccharide comprising N-acetyl  $\beta$ - $(1\rightarrow6)$ -glucosamine structures" or "polysaccharide comprising N-acetyl  $\beta$ - $(1\rightarrow 6)$ -glucosamine structures" refers to those structures found in the cell wall of microbes. The microbial wall contains a large number of these structures that are conserved across many microbial lines. These structures are predominantly N-acetyl  $\beta$ -(1 $\rightarrow$ 6)-glucosamine but include regions of deacetylated saccharides due to the action of enzymes such as poly-beta-1,6-D glucosamine-N-deacetylase. As such, the vaccines of this invention generate antibodies that comprise those that target such deacetylated oligosaccharide regions. Without being limited to any theory, antibodies against such deacetylated saccharides are cytotoxic *in vivo*  against such microbes.

**[0042]** The term "vaccine composition" as used herein refers to compositions comprising compounds of formula **I** and II above including adjuvants and a pharmaceutical carrier. These compositions can also comprise limited amounts of low molecular weight amino compounds including those wherein the amount of such amino compounds is no more than **3** weight percent based on the weight of the toxoid present and, preferably, less than 2 weight percent and, more preferably, less than **1** weight percent. These compositions provide effective immunity against any microbe that comprises oligosaccharides / polysacchariodes having N-acetyl-β-(1→6)-glucosamine structures in its cell wall. Thus, unlike classic vaccines that vaccinate against a single bacteria, the vaccine compositions described herein are capable of providing effective immunity against any microbe possessing the oligosaccharide structure described herein. Such microbes include, without limitation, Gram-positive bacteria, Gram-negative bacteria, antibiotic resistant bacteria (e.g., methicillin resistant *Staphylococcus aureus),* fungi, and the like.

**[0043]** The term "effective immunity" as used herein refers to the ability of a defined amount of the vaccine composition to generate an antibody response *in vivo* that is sufficient to treat, prevent, or ameliorate a microbial infection wherein said microbe contains oligosaccharides / polysaccharides comprising N-acetyl-B-(1->6)-glucosamine in its cell walls.

**[0044]** The vaccines compounds refer to the compounds of formula **I** and II. These compounds may exist as solvates, especially hydrates. Hydrates may form during manufacture of the compounds or compositions comprising the compounds, or hydrates may form over time due to the hygroscopic nature of the compounds. Compounds of this invention may exist as organic solvates as well, including DMF, ether, and alcohol solvates among others. The identification and preparation of any particular solvate is within the skill of the ordinary artisan of synthetic organic or medicinal chemistry.

**[0045]** The term "toxoid" refers to monomeric and oligomeric tetanus toxoid forms. The presence of oligomeric tetanus toxoid components reduces the average number of exposed reaction amino groups as the surface area of each monomeric toxoid in the oligomer is reduced **by** oligomerization. In turn, this results in lower factors for the oligosaccharide bound to the toxoid.

**[0046]** "Subject" refers to a mammal. The mammal can be a human or non-human mammal but preferably is a human.

**[0047]** "Treating" or "treatment" of a disease or disorder in a subject refers to **1)**  preventing the disease or disorder from occurring in a subject that is predisposed or does not yet display symptoms of the disease or disorder; 2) inhibiting the disease or disorder or arresting its development; or **3)** ameliorating or causing regression of the disease or disorder.

**[0048]** "Effective amount" refers to the amount of a vaccine composition of this invention that is sufficient to treat the disease or disorder afflicting a subject or to prevent such a disease or disorder from arising in said subject or patient.

**[0049]** "Reactive amino functional group" refers to a primary amino groups **(-NH2)** that are found on lysine and guanidine side chains of tetanus toxoid but do not include amido **(-NHC()-)** groups found in peptide linkages or amido side chains of tetanus toxoid such as that found in glutamine.

**[0050]** "Low molecular weight amino compounds" refer to amino containing compounds that are present as contaminants in a tetanus toxoid composition including fragments of the toxoid, buffers containing amino groups, reaction quenchers such as lysine, ammonium sulfate, and the like, toxin detoxifying agents such as formalin, and other amino containing reagents that have been in contact with the tetanus toxoid. Typically such low molecular weight reactive amino compounds have a molecular weight of less than about **10,000** and preferably less than **1,000.** In one embodiment, such low molecular weight amino compounds are identified **by** the elution peak in Figure **3.** 

#### **General Synthetic Methods**

**[0051]** The compounds of this invention can be prepared from readily available starting materials using the following general methods and procedures. It will be appreciated that where typical or preferred process conditions (i.e., reaction temperatures, times, mole ratios of reactants, solvents, pressures, etc.) are given, other process conditions can also be used unless otherwise stated. Optimum reaction conditions may vary with the particular reactants or solvent used, but such conditions can be determined **by** one skilled in the art **by** routine optimization procedures.

**[0052]** Additionally, as will be apparent to those skilled in the art, conventional protecting groups may be necessary to prevent certain functional groups from undergoing undesired reactions. Suitable protecting groups for various functional groups as well as suitable conditions for protecting and deprotecting particular functional groups are well known in the art. For example, numerous protecting groups are described in T. W. Greene and P. **G.** M. Wuts, *Protecting Groups in Organic Synthesis,* Third Edition, Wiley, New York, **1999,** and references cited therein.

**[0053]** The starting materials for the following reactions are generally known compounds or can be prepared **by** known procedures or obvious modifications thereof. For example, many of the starting materials are available from commercial suppliers such as SigmaAldrich (St. Louis, Missouri, **USA),** Bachem (Torrance, California, **USA),** Emka-Chemce (St. Louis, Missouri, **USA).** Others may be prepared **by** procedures, or obvious modifications thereof, described in standard reference texts such as *Fieser and Fieser's Reagentsfor Organic Synthesis,Volumes* **1-15** (John Wiley, and Sons, **1991),** *Rodd's Chemistry of Carbon Compounds,* Volumes **1-5,** *and Supplementals* (Elsevier Science Publishers, **1989),** *Organic Reactions,Volumes* 1-40 (John Wiley, and Sons, **1991),** *March's Advanced Organic Chemistry,* 

(John Wiley, and Sons, 5th Edition, 2001), and *Larock's Comprehensive Organic Transformations* (VCH Publishers Inc., **1989).** 

#### **Synthesis of Representative Vaccine Compounds of the Invention**

**[0054]** The general synthesis of the vaccine compounds of this invention are known in the art and are disclosed in **US** Patent Application Serial No. **10/713,790** as well as in **US**  Patent Nos. **7,786,255** and 8,492,364 each of which are incorporated herein **by** reference in its entirety.

**[0055]** In one embodiment for the vaccine compounds described herein, the  $\beta$ - $(1\rightarrow6)$ glucosamine group is limited to from 4 to **6** units and preferably **5** units, *e.g., y* **=** 2 to 4 in formulas I-III.

**[0056]** In some embodiments, the compounds are homogeneous in that **y** is a single integer selected from **1** to **10,** inclusive. Thus, compounds disclosed herein may be designed to be homogeneous with **y =** to **1,** 2, **3,** 4, **5, 6, 7, 8, 9,** or **10.** In some embodiments, compounds of formula **I** may be designed to be heterogeneous with two or more values for **y**, such as a mixture of  $y = 1$  and 2, or  $y = 2$  and  $y = 3$ , or  $y = 3$  and  $y = 4$ , or  $y = 4$  and  $y = 5$ , or  $y = 5$  and  $y = 6$ , or  $y = 6$  and  $y = 7$ , or  $y = 7$  and  $y = 8$ , or  $y = 8$  and  $y = 9$ , or  $y = 9$  and  $y = 10$ . Such pairings of **y** need not be contiguous. Thus, compounds may include mixtures of **y = 1**  and  $y = 3$ , or  $y = 1$  and  $y = 4$ , or  $y = 2$  and  $y = 4$ , or  $y = 2$  and  $y = 5$ , and so on in any combination of 2 or more different values for **y.** In some embodiments, compounds may be heterogeneous with **3** or more values for **y,** or 4 or more values for **y,** or **5** or more values for **y,** up to all **10** different values for **y.** In some embodiments, each incidence of **y** is independent in compounds of formula I.

**[0057]** In some embodiments, two or more compounds of formula **I** may be used in a pharmaceutical composition in which each individual compound of formula **I** is homogeneous in **y,** while the other compound(s) of formula **I** has/have a different **y** value. In such an embodiment, the homogenous compounds employed are simply mixed together at a defined weight percentage. For example, a pharmaceutical composition may comprise a compound of formula **I** in which **y =1** in a mixture with a compound of formula **I** in which **y** is 2. When pharmaceutical compositions or methods include a heterogenous mixture of compounds of formula I, the mixture can be one that is defined in terms of the relative weight percentages of each compound of formula I. For example, the mixture can include

**50** weight percent of a compound of formula **I** with **y** equal to **1** and **50** weight percent of a compound of formula **I** with **y** equal to 2. Any combination of compounds totaling **100%** is contemplated, for example, **1,** 2, **3** 4, **5** or more compounds each with a different **y** value can be mixed with known relative weight percents totaling **100%.** Accordingly, any combination of weight percentages of compounds of formula **I** can be used in the pharmaceutical compositions and methods disclosed herein. Thus, for a combination of two compounds of formula I, the percentage can be expressed as a ratio of the two compounds and can be in any range from **0.1:99.9** to **99.9:0.1,** inclusive, and any values there between, such as **1:99, 5:95, 10:90, 15:85, 20:80,** and so on up to **99:1,** including fractional values. Similarly, when 3,4, **5,** or more compounds of formula **I** in a pharmaceutical composition are used, the relative weight percentages of each compound can vary from **0.1** weight percent to a maximum of **99** weight percent provided that the total amount of the different compounds of formula **I** add up to **100%.** 

**[0058]** The formation of the linker group is achieved **by** art recognized synthetic techniques exemplified but not limited to those found in **US** Patent No. 8,492,364 and the examples below. In one embodiment, a first portion of the aglycon is attached to the reducing f-(1->6)-glucosamine unit retains a thiol **(-SH)** group as depicted below in formula **III:** 



where y is an integer from 1 to 10 and optionally no more than 40% of the amino groups are N-acetyl groups.

**[0059]** The second portion of the linker is attached to the tetanus toxoid in the following manner as depicted in formula IV.



**[0060]** In this formula, separate parts of tetanus toxoid are depicted **by** squiggly lines and are only illustrative in nature and are not intended to provide a complete structure of the toxoid. Any disulfide bridge is represented **by** a single line connecting the parts. For the sake of clarity, only a single second portion of the linker is illustrated whereas there are multiple such second portions covalently attached to amino groups found on the toxoid.

**[0061]** When the first and second portions of the linker are combined under coupling conditions, a thioether linkage is formed. The reaction is conducted in an inert diluent optionally in the presence of a base so as to scavenge the acid generated. The thioether linkage connects the first and second portions of the linker thereby providing for covalent linkage of the tetanus toxoid to the oligosaccharide  $\beta$ -(1 $\rightarrow$ 6)-glucosamine group through the combined linker as illustrated below for a vaccine compound where **y** is as defined herein.



wherein no more than 40% of the amino groups are optionally N-acetyl groups.

**[0062]** It being understood that the number of  $\beta$ -(1 $\rightarrow$ 6)-glucosamine group-linkergroups attached to the tentatus toxoid are stoichiometrically controlled so that about **31** to

about **39** of such groups are bound to the toxoid thereby providing for the vaccine compounds of this invention.

#### **Methods, Utility and Pharmaceutical Compositions**

**[0063]** The vaccine compositions of this invention are capable of initiating an effective immune response against microbes that possess PNAG oligosaccharide  $\beta$ - $(1\rightarrow6)$ glucosamine structures in their cell walls. After inoculation of a patient, an effective immune response develops about 4 weeks later. After an effective immune response develops, the patient is provided with protection against subsequent microbial infections wherein the offending microbes have cell walls comprising **PNAG.** 

**[0064]** When so used, a vaccine composition of this invention is administered to patients at risk of a microbial infection arising from such microbes. Such patients include, **by** way of example only, those who are elderly, those with upcoming elected surgeries, those traveling to destinations where there is an outbreak of microbial infections, and the like. The vaccine is typically administered to an immune competent patient intramuscularly with a suitable adjuvant to enhance the immune response. After the latency period has passed, the patient has acquired natural immunity against such microbes. Such immune competent patients have an effective immune system that can generate an immune response to an antigen. Preferably, such patients have active white blood count (WBC) of at least about **1000** WBC per microliter, preferably at least about **1500** WBC per microliter, more preferably at least about 2000 WBC per microliter, even more preferably, about **3000** WBC per microliter and, most preferably, about 4000 WBC per microliter.

**[0065]** In another embodiment, the vaccine compositions of this invention can be used therapeutically particularly when the microbial infection is localized and/or non-life threatening. In such a case, a vaccine composition of this invention is administered to patients suffering from a microbial infection arising from such microbes. The vaccine is typically administered to an immune competent patient intramuscularly with a suitable adjuvant to enhance the immune response. Upon administration, effective immunity is generated within about 4 weeks. **If** the patient is still suffering from the infection, the natural immunity arising from the vaccine facilitates recovery.

**[0066]** When so used, the vaccine compositions of this invention are administered in a therapeutically effective amount **by** any of the accepted modes of administration for agents that serve similar utilities. The actual amount of the vaccine compound of this invention, i.e., the active ingredient, will depend upon numerous factors such as the severity of the disease to be treated, the age and relative health of the subject, the potency of the vaccine compound used, the route and form of administration, and other factors well-known to the skilled artisan.

**[0067]** An effective amount or a therapeutically effective amount of a vaccine compound of this invention, refers to that amount of vaccine compound that results in a sufficient titer of antibodies so as to ameliorate symptoms or a prolongation of survival in a subject. Toxicity and therapeutic efficacy of such vaccine compounds and vaccine compositions can be determined **by** standard pharmaceutical procedures in cell cultures or experimental animals.

**[0068]** The vaccine compositions described herein are typically administered as an injectable sterile aqueous composition that comprise one or more conventional components well known in the art including, **by** way of example only, adjuvants, stabilizers, preservatives and the like.

#### *COMBINATIONS*

**[0069]** The vaccine compounds and compositions of this invention can be used in conjunction with other therapeutic compounds or other appropriate agents as deemed suitable **by** the attending clinician. In selected cases, the vaccine compound of this invention can be concurrently administered with antibiotics for treating a bacterial infection as well as agents that enhance the immune response induced **by** the vaccine compound and/or composition. In the case of antibiotics, the selection of the appropriate antibiotic or cocktail of antibiotics and the amount to be administered to the patient is well within the skill of the attending physician based on the specifics of the offending bacteria, the extent of bacterial infection, the age, weight, and otherwise relative health of the patient. As is appropriate, the attending physician may co-administer an immune boosting drug or adjuvant in combination with the vaccines described herein.

**[0070]** The vaccine compositions of the invention may be administered with an adjuvant that potentiates the immune response to the antigen in the patient. Adjuvants include but are not limited to aluminum compounds such as gels, aluminum hydroxide and aluminum

phosphate, and Freund's complete or incomplete adjuvant (e.g., in which the antigen is incorporated in the aqueous phase of a stabilized water in paraffin oil emulsion. As is apparent, the paraffin oil can be replaced with other types of oils such as squalene or peanut oil. Other materials with adjuvant properties include **BCG** (attenuated *Mycobacterium tuberculosis)* calcium phosphate, levamisole, isoprinosine, polyanions (e.g., **polyA:U),** lentinan, pertusis toxin, lipid **A,** Saponins, **QS-21** and peptides, e.g., muramyl dipeptide, and immuno stimulatory oligonucleotides such as **CpG** oligonucleotides. Rare earth salts, e.g., lanthanum and cerium, may also be used as adjuvants. The amount of adjuvant used depends on the subject being treated and the particular antigen used and can readily determined **by** one skilled in the art.

# **EXAMPLES**

**[0071]** This invention is further understood **by** reference to the following examples, which are intended to be purely exemplary of this invention. This invention is not limited in scope **by** the exemplified embodiments, which are intended as illustrations of single aspects of this invention only. Any methods that are functionally equivalent are within the scope of this invention. Various modifications of this invention in addition to those described herein will become apparent to those skilled in the art from the foregoing description and accompanying figures. Such modifications fall within the scope of the appended claims.

**[0072]** The following terms are used herein and have the following meanings. **If** not defined, the abbreviation has its conventionally recognized definition.





# *Example 1* **-** *Tentanus Toxoid Preparation*

**[0073]** Samples of crude tetanus toxoid comprising monomeric toxoid comprising at least 25 and preferably at least **31** free amino groups were concentrated and chromatographed on a Superdex® 200 size exclusion column using two different loadings  $-$ **0.6%** and 1.2% of the column bed volume (commercially available from SigmaAldrich, St. Louis Missouri, **USA).** The elution profiles were monitored **by A280** absorbance. As shown in Figure **3,** six distinct peaks (pools **1-5** and the monomer pool) were observed with the purported monomer fraction representing the largest peak area. Pools were created based on analytical **SEC** HPLC analysis of the individual fractions. The crude tetanus toxoid and each of the individual pools was analyzed **by SEC** HPLC and the results are summarized in Table **1** and in Figure **1.** 

Table **1 -** Analytical **SEC** HPLC Analysis /Quantification of Superdex 200 Pools





**[0074]** The monomer pool revealed a single symmetrical peak with an elution volume consistent with monomeric TT **(99.9** area%) and no additional peaks detected. Since the column load contained **58.8** area **%** monomer, this data confirmed the effectiveness of the preparative Superdex purification protocol under these conditions. The remaining fractions from the Superdex 200 column contained mainly larger molecular weight material (Pools **1 &** 2) or lower molecular weight species (Pools **3-5)** compared to the TT monomer when monitored **by SEC** HPLC. The mass balance for the overall process was assessed **by** protein recovery **(BCA)** and the results are summarized in Table 2.

Sample	Volume (mL)	Concentration	<b>Total Protein</b>	Total
		(mg/mL)	(mg)	Recovery
<b>ARMPCT</b>	60	5.7	342	
Concentrated TT	6.6	43.1	284.5	83%
Concentrated TT	$\overline{4}$	43.1	172.4	
for Prep SEC				
TT Monomer	40	2.2	88.0	51%
Pool				
Pool 1	8.0	0.1	0.8	0%
Pool 2	28.0	0.8	22.4	13%
Pool 3	36.0	0.9	32.4	19%
Pool 4	64.0	0.2	12.8	7%
Pool 5	18.0	$\boldsymbol{0}$	$\bf{0}$	0%
TT Monomer				
Pool for Form.	38.0	2.2	83.6	
Conc. TT				
Monomer at pH8	4.8	15.2	73.0	87%

Table 2 **-** Mass Balance from TT Monomer Purification **-** Formulation Based on Protein Recovery

It being understood that other size exclusion chromatographic procedures can be used to achieve the same result.

**[0075]** Protein recovery from the spin concentration step was **83%** with the losses mainly due to removal of smaller molecular weight proteins **/** peptide contaminants via the filtrate (data not shown). Following purification **by** preparative Superdex 200 chromatography, yield of the TT-monomer was **51%** with the remainder of the protein recovered in the higher molecular weight **/** aggregate and smaller molecular weight fractions. Finally, the TT-monomer was recovered in **87%** yield following buffer exchange into reaction buffer. For this example, the overall process recovery from crude tetanus toxoid to purified **/** formulated TT-monomer was **35%** based on protein recovery.

**[0076]** The stability of purified TT-monomer was assessed following storage at **pH 9.0 (40** or **-70°C)** or at **pH 7.5 (-70°C)** for up to 4 weeks. Specifically, the monomer content **(SEC**  HPLC) and protein concentrations were monitored at weekly intervals. The TT-monomer did not show a significant change in the **SEC** fingerprint or protein concentration over 4 weeks at 4C **(pH 9.0)** or frozen at **-70°C (pH 7.5** or **9.0).** Since this study utilized a limited set of stability indicating methods, the decision was made to purify the TT monomer in advance of each production campaign and to store the purified TT in reaction buffer **(50**  mM HEPES, pH 8.0) at 4°C and use it within 7 days of generation.

### **Example 2 - Attachment of SBAP to TT Monomer**

Step **1:** Preparation of **N-BABA:** 



**[0077]** Commercially available beta-alanine, compound **1,** is converted to **N-BABA**  (bromoacetyl-p-alanine), compound 2, **by** reaction with at least a stoichiometric amount of commercially available bromoacetyl bromide. In a first container,  $\beta$ -alanine is combined into water with sodium bicarbonate or other suitable base to scavenge the acid that will be generated during the reaction. The aqueous solution is mixed at about  $20 \pm 5^{\circ}$ C until a solution is obtained. The solution is then maintained at about  $5 \pm 5^{\circ}$ C. In a separate container, the requisite amount of bromoacetyl bromide is added followed **by** the addition of dichloromethane. The contents of the both containers are combined. After reaction completion, **6N HCl** is added and mixed to a **pH** approximately 2. The resulting **N-BABA** is extracted from the solution **by** a suitable solvent such as ethyl acetate. The organic layer is

concentrated under conventional conditions such as under vacuum at an elevated temperature such as **60°C.** Heptane is then added to precipitate **N-BABA** that is then collected on a filter and dried in a vacuum oven at 40°C. This product is used as is in the next step.

Step 2: Preparation of SBAP:



**[0078] N-BABA,** compound 2, is reacted with N-hydroxysuccinimide **(NHS)** under conventional conditions well known in the art to generate SBAP, compound **3.** Specially, **<sup>N</sup>** BABA is combined with at least a stoichiometric amount of **NHS** in a suitable inert solvent such as methanol, ethanol, isopropanol and the like. The resulting solution is stirred at about 20 **±5C** until a clear solution is obtained. N-Diisopropylcarbodiimide is then added to the reaction mixture and mix with the generation of solids. The system is then cooled to **0 ±5C** and resulting SBAP is provided **by** filtration. Further purification entails prechilling a mixture of isopropanol and heptanes and washing the filter cakes followed **by** drying wet cake in a vacuum oven at about 30°C. The resulting SBAP is used as is in the coupling reaction with the TT monomer.

**[0079]** Alternatively, SBAP can be prepared in the manner set forth in **US** Patent No. **5,286,846,** which patent is incorporated herein **by** reference in its entirety. Specifically, the method described therein is provided **by** the following synthetic scheme:



Step **3 -** Conjugation

**[0080]** Purified TT monomer, as described above, contains 43 lysine residues **/** mole as quantified **by** a free amine assay. Reaction of TT monomer with increasing concentrations of SBAP from **0** to **170** molar equivalents led to a corresponding decrease in the free amine content over the range **15-110** molar equivalents of SBAP. **A** steady state conversion was achieved at SBAP charges **>110** equivalents. Assuming that the loss of free amines is directly proportional to loading of SBAP linker, the linker density at saturation was estimated to be 43 moles SBAP **/** TT monomer. The monomer/aggregate content of the linker TT/monomer intermediate and protein concentration at each titration point was also assessed. The monomer content prior to linker addition was **99.7** percent and addition of increasing amounts of SBAP linker did not significantly change the monomer level (no aggregate detected). Also, the recover of protein across the titration steps was similar. Based on this collective data, a value of **110** molar equivalents of SBAP for **1** hour at ambient temperature was selected as appropriate reaction conditions for all subsequent syntheses.

# *Example 3 - Oligosaccharide Synthesis*

### Synthesis of Building Blocks

**[0081]** The reaction scheme below illustrates for the synthetic steps used to prepare compounds **3, 5** and **8** that are elaborated upon below.



### Synthesis of Compound **D.**

**[0082]** Commercially available 1,3,4,6-Tetra-0-acety-2-deoxy-2-N-phthalimido-p-D glucopyranoside, compound **C, (120.6 g, 252.6** mmol) and toluene (200 mL) were charged to a 1L Bichi flask and rotated at 40°C until dissolved **(<5** minutes). The solvents were

evaporated and to provide for a foam. Toluene (200 mL) was charged to the flask and rotated at 40°C until dissolved **(<5** minutes). The solvents were evaporated again until dry. **A** crystalline solid formed, sticking to the walls. Dichloromethane **(800** mL) was charged to the flask and rotated at ambient until dissolved; the resulting dark brown solution was charged to a 5L jacketed reactor and the flask was rinsed into the reaction with additional dichloromethane (200 mL). The heating/cooling jacket was set to **20°C** and the reactor contents were stirred mechanically. Ethanethiol (40 mL, 540 mmol) was dissolved in **50** mL dichloromethane and added to vessel and the flask rinsed with **50** ml dichloromethane into the vessel. Boron trifluoride diethyl etherate **(50** mL, **390.1** mmol) was dissolved in dichloromethane **(50** mL) and added to the reactor, rinsed with dichloromethane **(50** mL) and added to vessel. The mixture was stirred at **20°C** for 2h. The reaction was checked **by TLC** for residual **C.** Mobile phase was toluene: ethyl acetate **(3:1,** v/v), Product Rf **-** 0.45, **<sup>C</sup>** Rf **- 0.3** with **UV** visualisation. **If** significant amounts of **C** were present extended reaction time was required.

**[0083]** Stirring was set to a high speed and 4M aq. sodium acetate (1.25 L, **5100** mmol) was added. The phases were mixed well for **30** minutes. The **pH** of the aqueous layer was checked with a dipstick and confirmed to be **-pH=7.** Stirring was turned off and the reaction mixture was left standing for **70** minutes.

**[0084]** The layers were separated and collected. The organic layer (bottom layer, 1.2 L) and ethanol (840 mL, 14400 mmol) were charged to the reactor. The jacket was set to **60°C**  and solvent distilled under atmospheric pressure (dichloromethane **bp** 40 **°C** and ethanethiol **bp 35°C,** receiver flask in ice-bath). When the distillation slowed the jacket temperature was increased to **70°C.** After **1300** mL of distillate were collected, a sample of the vessel content was taken and the ratio of dichloromethane to ethanol determined **by**  1H-NMR and confirmed to be under **10** mol% dichloromethane. **If** more dichloromethane was present further distillation would be necessary. Additional ethanol was added (400 mL) followed **by** seed crystals of **D.** The jacket was cooled to **5°C** over **30** minutes. The crystal slurry was stirred for **3** days at **5 °C.** The solids were collected on a sintered funnel and washed with petroleum ether **(60-80°C):** 1x **500** mL slurry, 1x **300** mL plug. The solids were transferred to a **500** mL RBF and dried to constant weight (over -4h) on a rotary evaporator (bath temperature 45°C) providing an off-white solid. Expected Yield: **-86 g (71%** from **C).** 

### Synthesis of Compound **1**

**[0085]** Anhydrous methanol **(33** mL) was charged to a **50** mL round bottom flask. Sodium methoxide in methanol **(30%** solution, 25 pL, **0.135** mmol) was added and the resulting solution was stirred at ambient temperature for **5** minutes. Ethyl 3,4,6-tetra-O acetyl-2-deoxy-2- N-phthalimido-p- thio-D-glucopyranoside (compound **D) (3.09 g,** 6.44 mmol) was added in portions  $\left(\frac{200}{2}\right)$  over 10 minutes, at a rate that allowed the solids to dissolve during addition. The reaction was stirred at ambient temperature for 2.5 h. **TLC**  (EtOAc) showed complete consumption of compound **D** (Rf **= 0.9)** and formation of one, more polar spot: Rf **= 0.5. A** sample was taken and submitted for reaction completion **IPC by**  HPLC (2.5L reaction mixture in **0.8** mL acetonitrile and 0.2 mL water), pass condition was **NMT 1.00** area% Compound **D.** Acetic acid was added **(8** pL, **0.1397** mmol). The **pH** was checked with a dipstick and confirmed to be **-pH 5-6.** The mixture was concentrated on a rotary evaporator **(50°C)** to near dryness. EtOAc **(15** mL) was added and the majority evaporated. The residue was dissolved/slurried in **15** mL EtOAc and removed from the rotary evaporator. 2 mL petroleum ether was added and the mixture was stirred at ambient temperature. The crystal slurry was stirred overnight. The solids were collected on a sintered funnel, washed with petrol (2 x **10** mL) and dried on rotary evaporator (45°C bath temperature) to constant weight. Expected Yield: 1.94 **g (85%** from Compound **D).** 

#### Synthesis of Compound 2

**[0086]** Compound **1** (2.040 **g)** was dissolved in pyridine **(28** mL) and the solution concentrated to approximately half the volume  $(\sim 14 \text{ mL})$  in a rotary evaporator at  $40^{\circ}$ C bath temperature to give a yellow solution. More pyridine was added (14 mL) and again the solution concentrated to approximately 14 mL in the same manner. The solution was placed under argon and trityl chloride **(2.299 g, 1.36** eq) was added before an air-cooled condenser was attached and the solution heated to **50 °C** with stirring. After 4 hours an **IPC**  was run (HPLC; **5** tL into **800** pL MeCN, residual compound **1 NMT 3.00** area%). As soon as the **IPC** was met the reaction was cooled to **10-15 °C.** Benzoyl chloride **(1.60** mL, 2.34 eq) was added dropwise over a period of 20 minutes keeping the reaction temperature below 20 **°C.** Once addition was complete, the reaction was allowed to warm to ambient temperature and stirred for at least **3** h. At this time an **IPC** was run (HPLC; **5** pL into **1500**  tL MeCN, residual mono-Bz derivatives of compound **1 NMT 3.00** area% total). As soon as the **IPC** was met the reaction was cooled to **0 °C** and quenched **by** the slow addition of

methanol **(0.8** mL), ensuring the reaction temperature remains below 20 **°C.** The quenched reaction was then warmed to ambient temperature.

**[0087]** The product mixture was diluted with toluene (20 mL) and stirred for **1** hour at ambient temperature before the precipitate was removed **by** filtering through a sintered funnel. The toluene solution was then washed with citric acid  $(20\% \text{ w/w}, 4 \text{ x } 20 \text{ mL})$ followed **by** saturated NaHC03 **(9 %** w/v, 20 mL) which resulted in a minor reaction with any residual citric acid present. The toluene (upper) layer was then washed with brine (20 mL) before being evaporated in a rotary evaporator at 40°C bath temperature to give a yellow/orange syrup (6.833 g). The syrup was submitted for IPC (H<sup>1</sup> NMR, pass condition **NMT 30** wt% residual toluene). Expected Yield: **-6.833 g** (147 **%).** 

# Synthesis of Compound **3**

**[0088]** Glacial acetic acid (648 mL) and ultrapure water **(72** mL) were mixed together to give a **90 %** acetic acid solution. **A** portion of the acetic acid solution **(710** mL) was added to crude compound 2 **(111 g)** along with a stirrer bar. An air cooled condenser was attached to the flask and the mixture was then heated to **70°C.** Due to the viscous nature of 2, the mixture was not fully dissolved until **1** hour and 20 minutes later, at which point stirring began. After 2 hours an **IPC** was run (HPLC; **5** tL into **800** pL MeCN, residual compound 2 **NMT 3.00** area%). As soon as the **IPC** met the specs, the reaction was cooled to ambient temperature. The mixture was transferred to a sintered funnel and the precipitated trityl alcohol **(31.09 g)** filtered off using house vacuum. The flask was rinsed with a further portion of **90%** acetic acid (40 mL) and the total washings transferred to a mixing vessel. Toluene **(700** mL) and water **(700** mL) were added and mixed thoroughly. The aqueous (lower) layer was a cloudy white solution and was tested for **pH** (it was expected to be **<** 2). The wash was repeated twice more with water (2 x 700 mL; pH of  $\sim$  2.4 and  $\sim$  3 respectively, colorless clear solutions). Saturated NaHC03 **(9 %** w/v, **700** mL) was added to the mixing vessel resulting in a minor reaction (gas evolution). The toluene (upper) layer was then washed with brine **(700** mL) before being evaporated in a rotary evaporator at 40°C bath temperature to give a yellow/orange solid/liquid mixture **(86 g).** This mixture was dissolved in 400 mL toluene **(300** mL **+ 100** mL washings) and loaded on to a silica column (450 **g** silica) which was equilibrated with **3** column volumes **(CV)** of petroleum ether:toluene **(1:1,** v:v). The column was eluted using a stepwise gradient, fractions of **1 CV (790** mL) were collected. The gradient used was:

4 vol% ethyl acetate in petroleum ether:toluene **(1:1** v:v, 4 CVs) **<sup>M</sup> 8** vol% ethyl acetate in petroleum ether:toluene **(1:1** v:v, 12 CVs) **<sup>M</sup> 15** vol% ethyl acetate in petroleum ether:toluene **(1:1** v:v, 4 CVs) **<sup>M</sup>** 20 vol% ethyl acetate in petroleum ether:toluene **(1:1** v:v, (4 CVs) **<sup>M</sup> 30** vol% ethyl acetate in petroleum ether:toluene **(1:1** v:v, **1 CV) M** 

**[0089]** The product eluted over 14 fractions. **TLC** was used to locate the product containing fractions. **All** fractions were submitted to **IPC** (HPLC, **NMT 1.50** area% of the peak at 10.14 minutes and **NMT 1.50** area% of the peak at 10.94 mins). Fractions not meeting **IPC** were set aside for processing to compound 4. The combined fractions were evaporated in a rotary evaporator at 45°C bath temperature to give a colorless syrup. Expected Yield: **-60 g, (78 %).** 

# Synthesis of Compound 4

**[0090]** Crude compound  $3$  (39.54 g, containing  $\sim$  21 g of compound  $3, \sim 37$  mmol, taken just prior to chromatography of **3)** was dissolved in toluene **(7.2** mL) and dry pyridine (14.2 mL, **176** mmol, -4.8 eq.) added to give a homogenous solution. Acetic anhydride **7.2** mL **(76**  mmol,  $\sim$ 2.1 eq.) was added and the mixture stirred for 18 h at 25 $^{\circ}$ C. *During the reaction* solids precipitate, some of this precipitate was likely to be compound 4. The reaction was sampled for **IPC,** if the amount of compound **3** detected was **> 1.00** area **%** then further charges of dry pyridine (1.4 mL, **17** equivs) were added and the reaction continued until residual compound **3** was **1.00** area **%** in the liquid phase.

**[0091]** The reaction was diluted with dichloromethane (112 mL) then water **(2.8** mL) and methanol **(2.8** ml) were added. The mixture was stirred for **3** h at 25 **°C.** This stir period was shown sufficient to quench the excess acetic anhydride. The mixture was washed with citric acid monohydrate/water **20/80** w/w (112 mL). The aqueous phase was back extracted with dichloromethane **(50** mL). The dichloromethane that was used for the back extract was set aside and used to back-extract the aqueous phases from the remaining citric acid washes. The main dichloromethane extract was returned to the vessel and the citric acid washing process repeated until the **pH** of the aqueous phase was 2 (typically two further washes). The combined citric acid washes were back-extracted. The back-extract and main dichloromethane extract were then combined. The resulting dichloromethane solution was washed with **5%** w/v NaHC03 **(100** mL), the dichloromethane phase was taken and washed with water **(100** mL). The dichloromethane phase was transferred to an

evaporating vessel and ethyl acetate **(50** mL) was added and the solution concentrated to a syrup.

**[0092]** Ethyl acetate **(150** mL) was added and the product dissolved **by** heating to **55°C**  with stirring. Petroleum ether **60-80** (200 mL) was added and the solution re-heated to **55°C** and held for **5** min. The solution was cooled to 45°C and seed crystals **(30** mg) added, it was then cooled to **18°C** over **3** h with stirring and held at **18°C** for at least **1** h. The crystals were collected **by** filtration and washed with ethyl acetate/petroleum ether (1/2 v/v, **60** mL). Drying *in vacuo* afforded compound 4 (16.04 **g, 77%** from 2). Expected Yield: **16.0 g (77 %** from Compound 2).

# Synthesis of Compound **3.1**

**[0093]** 3-aminopropan-1-ol **(7.01 g, 93** mmol) was dissolved in **DCM (70** mL) and cooled to **0°C.** Benzyl chloroformate (5.40 mL, **32** mmol) was dissolved in **DCM** (20 mL) and added dropwise keeping the internal reaction temp below **10°C.** Once complete, the flask was stirred at room temperature for 2 h. **A** sample removed for NMR analysis **(IPC:** 20 ML **+ 0.6**  mL **d6-DMSO)** indicated that the benzyl chloroformate reagent had been consumed. The product mixture was then washed with citric acid **(10%** w/w, 2 x **90** mL), water **(90** mL) and brine **(90** mL). The **DCM** (lower) layer was then evaporated in a rotary evaporator at 40 **°C** bath temperature to give a slightly cloudy oil/liquid (6.455 **g).** This oil was dissolved in ethyl acetate **(7** mL), warming to 40 **°C** if necessary to dissolve any precipitated solid, and then allowed to cool to room temperature. Petroleum ether (4 mL) was added slowly to the stirring solution along with a seed crystal, at which point the product started crystallizing slowly. Once the majority of the product had precipitated, the final portion of petroleum ether **(17** mL) was then added slowly (total solvent added: ethyl acetate:petroleum ether **1:3,** 21 mL). The product was then filtered under vacuum and washed with petroleum ether (5 mL) to give the product as a fine white powder  $(4.72 \text{ g})$ . Expected Yield:  $\sim$ 4.7  $\text{g}$   $(61 \text{ %})$ .

#### Synthesis of Compound **5**

**[0094]** Compound 4 **(1.05 g, 1.73** mmol) was dissolved in dry acetone (12 mL, **0.06**  w/w water) and water **(39** pL, 2.15 mmol, **1.3** eq.) at ambient temperature. The solution was then cooled to **-10°C. NBS (0.639 g, 3.59** mmol, **2.08** eq.) was added in one portion. An exotherm in the order of **+7°C** was expected and the solution was then immediately re cooled to **-10°C. 15** minutes after the **NBS** addition, the reaction mixture was submitted for **IPC** (HPLC, pass condition less than 2.00 area **%** compound 4 remaining). **If** the reaction

was not complete, **1.00** eq. of **NBS (0.307 g, 1.73** mmol, **1.00** eq.) was added in one portion, the reaction was then held at **-10°C** for another **15** minutes and a further **IPC** carried out. The reaction was quenched **by** adding aqueous NaHCO3 **(5%** w/v, **5** mL) and cooling was stopped and the mixture allowed to warm to **10-20°C** during the following additions. After **3-5** minutes of stirring, further aqueous NaHC03 **(5%** w/v, **5** mL) was added and stirring continued for **5** minutes. **A** final aliquot of aqueous NaHC03 **(5%** w/v, **10** mL) was added with stirring followed **by** sodium thiosulfate (20% w/v, **5** mL). The mixture was stirred for 20 min. at **10-20°C** and the solids were then collected **by** filtration. The vessel was rinsed onto the filter pad with NaHC03 **(5%** w/v, 25 mL) and this rinse was filtered off. The filter cake was then rinsed successively with NaHC03 **(5%** w/v, 25 mL) and then water (25 mL). The (still-damp) filter cake was dissolved in **DCM** (20 mL) and washed with two lots of NaHC03 **(5%** w/v, 20 mL) and then once with water (20 mL). The dichloromethane layer was dried **by** rotary evaporation and then dissolved in ethyl acetate **(36** mL) at **65°C.**  Petroleum ether **60-80 (10** mL) was then added slowly with stirring and the mixture cooled to 45°C and stirred at 45°C for **30** min. Additional petroleum ether **60- 80** (22 mL) was added with stirring and the stirred mixture cooled to **15°C** over 2h. The product was collected **by** filtration, washed with petroleum ether/ethyl acetate 2/1 v/v (20 mL) and then dried under vacuum to give compound **5 (0.805** *g,* **83%** yield, a and **p** anomers combined purity **by** HPLC was **98%).** 

# Synthesis of Compound **7**

**[0095]** Compound 4 **(500** mg) and intermediate **3.1** (211 mg, 1.2 eq.) were weighed into a dry flask, toluene **(5** mL) was added and the solution concentrated on a rotary evaporator (45°C bath temperature). This was repeated once more before the starting materials were concentrated from anhydrous **DCM (5** mL). Once all of the solvent was removed, the residual solid was dried under vacuum for **10** minutes. Following drying, the starting materials were placed under argon, dissolved in anhydrous **DCM (5.0** mL) and activated 4A molecular sieves (450 mg, pellet form) were added. At this point, the **NIS** reagent was placed under high-vacuum to dry. After **10** minutes, the dried **NIS** (400 mg, 2.0 equivalents) was added and the solution stirred at room temperature for **30** minutes. **TMSOTf (8** pL, **5**  mol%) was then added quickly, which results in the solution changing from red/orange to a deep red/brown color. The reaction temperature also rose from 22 to **27 °C.** As soon as the **TMSOTf** was added an **IPC** was run for information only (HPLC; **10** pL into **1** mL MeCN-H20

**(8:2)).** The reaction was then quenched **by** the addition of pyridine (20 pL, 0.245 mmol) and stirred at ambient temperature for **5** minutes. The **DCM** solution was filtered to remove the molecular sieves and then washed with **10%** Na2S23 **(3** x **5** mL), brine (5 mL) and then concentrated on a rotary evaporator  $(40^{\circ}$ C bath temperature) to give crude compound **7** as a foamy yellow oil **(616** mg). Expected Yield: **-616** mg, **(99 %).** 

# Synthesis of Compound **8**

**[0096]** Crude compound **7 (16.6 g)** was dried **by** evaporation from toluene (2 x **30** mL) then from anhydrous **DCM (30** mL) to produce a yellow foam/oil. The flask was then placed under an argon atmosphere before anhydrous **DCM (100** mL) and dry MeOH **(260** mL) was added and the mixture stirred. The flask was then cooled to **0°C.** Acetyl chloride **(3.30** mL, 2.0 eq.) was added dropwise while maintaining an internal temp of less than **10°C.** Once addition was complete, the mixture was stirred at ambient temperature for **16** hours. At this point an **IPC** was run (HPLC; 20 pL into **1** mL MeCN, residual compound **7** no more than **3** area **%).** The flask was then cooled to **0°C** and the **pH** of the product solution adjusted to **pH 6.5-7.5 by** the addition of N-methylmorpholine **(7.0** mL total required). The product mixture was diluted with **DCM (50** mL) and washed with H20 (2 x 200 mL). The second H20 wash was cloudy and contained target material **by TLC** so this was back-extracted with **DCM (50** mL). The combined **DCM** layers were then washed with brine **(8** mL) before being evaporated in a rotary evaporator at 40°C bath temperature to give an off-white foam/oil **(-16.8 g).** This mixture was dissolved in 140 mL toluene **(100** mL **+** 40 mL washings) and loaded onto a silica column **(85 g** silica) which was equilibrated with **3** column volumes **(CV)** of **30** vol% ethyl acetate in petroleum ether. The column was eluted using a stepwise gradient, fractions of **1 CV** (140 mL) were collected. The gradient used was:

**30** vol% ethyl acetate in petroleum ether **(3** CVs) M **35** vol% ethyl acetate in petroleum ether (4 CVs) M 40 vol% ethyl acetate in petroleum ether **(9** CVs) M 50 vol% ethyl acetate in petroleum ether (4 CVs) <sup>[2]</sup> **60** vol% ethyl acetate in petroleum ether **(3** CVs) M

The product eluted over 12 fractions. **All** fractions were submitted to **IPC** (HPLC, **NMT 1.50**  area% of any impurity peak at **230** nm). The combined fractions were evaporated in a rotary evaporator at 40°C bath temperature to give an off-white foam which solidified to afford **8** as a crunchy solid (10.45 **g).** Expected Yield: 10.45 **g (66 %). <sup>M</sup>**

#### *Example 4 - Synthesis of Disulfide (Compound 17)*



Compound 17

The overall synthetic procedure for the synthesis of compound 17 is described in  $[0097]$ the synthetic scheme below.



# Synthesis of Compound 9

 $[0098]$ Compound 5 (1620 g, 1.18 eq.) and toluene (18 kg) were charged to a 50 L Büchi bowl in that order. The bowl was warmed in a water bath with a setting of  $50 \pm 10^{\circ}$ C for 30

min. Evaporation was run under vacuum using a water bath temperature of  $50 \pm 10^{\circ}$ C until no more solvent distilled. The water bath was cooled to 20 ± 10°C. Trichloroacetonitrile **(7.1 kg,** 21 equiv.) and dry **DCM (6.5 kg)** were charged to the bowl under nitrogen atmosphere. **A** suspension of sodium hydride **(5.6 g, 0.060** equiv.) in dry **DCM** (250 **g)** was charged to the bowl under nitrogen atmosphere. The bowl contents were mixed **by** rotation for 1  $\cdot$  2 h with a water bath temperature of 20  $\pm$  10°C. Compound 5 dissolved during the reaction. The bowl contents were sampled and submitted for reaction completion IPC (H<sup>1</sup> NMR, integrating triplet peak at 6.42 ppm (product) relative to triplet at **6.35** ppm (starting material); pass condition **5 %** residual starting material). Compound **3 (1360 g, 2.35** mol), dry **DCM (12.3 kg)** and powdered molecular sieves 4A **(136 g)** were charged to the **50** <sup>L</sup> reactor in that order. The reactor contents were mixed for 24 h. The reactor contents were sampled through a syringe filter and analyzed **by** Karl Fisher **(AM-GEN-011,** pass condition  $\leq$  0.03 %w/w). After reaching the moisture threshold ( $\sim$ 24 h), the reactor contents were adjusted to **0 ±5C.** The contents of the Bichi bowl were transferred to the reactor header as volume allowed. **A** solution of trimethylsilyl trifluoromethanesulfonate **(100 g, 0.18** eq.) in dry **DCM** (1250 **g)** was charged to the reactor under a nitrogen atmosphere. The header contents were drained to the reactor maintaining the reactor contents at  $0 \pm 10^{\circ}$ C throughout the addition. Addition took **15 -** 20 min. Dry **DCM** (1250 **g)** was charged to the Büchi bowl and then transferred to the reactor header. The header contents were drained to the reactor maintaining the reactor contents at **0 ±10<sup>0</sup> <sup>C</sup>**throughout the addition. The reactor contents were stirred at  $0 \pm 5^{\circ}$ C for 60 min. The reactor contents were sampled for reaction completion using **IPC** (HPLC, pass criteria **5 %** starting material). The reaction was quenched **by** charging N-methylmorpholine **(85 g, 0.36** eq.) to the reactor. The reactor contents were sampled for quench completion using **IPC** (wetted **pH** paper, pass criteria **pH 7).** Silica gel (4.9 **kg)** was charged to the Bichi bowl. The reactor contents were transferred to the Bichi bowl. Evaporation was run under vacuum using a water bath temperature of 40 **±10<sup>0</sup> <sup>C</sup>**until no more solvent distilled. Silica gel (1.4 **kg)** was charged to the Bichi bowl followed **by** dichloromethane **(7.0 kg)** used to rinse the reactor. The bowl contents were rotated to ensure solids were not adhered to the bowl surface. Evaporation was run under vacuum using a water bath temperature of 40 **±10<sup>0</sup> <sup>C</sup>**until no more solvent distilled. The bowl contents were divided into three portions for silica gel chromatography. **A 150** L KP-SIL cartridge was installed in the Biotage system. Ethyl acetate **(7.8 kg)** and petroleum ether (22 **kg)** were charged to the **50** L reactor along with **1/3** of the reaction

mixture adsorbed onto silica gel, mixed thoroughly and then transferred to a Biotage solvent reservoir. The solvent reservoir contents were eluted through the column so as to condition the column. The eluent was collected in 20 L jerry cans and discarded. The column was run in three batches and each was eluted with ethyl acetate/petroleum ether as described below:

- a. Ethyl acetate **(1.6 kg)** and Petroleum ether (4.4 **kg)** were charged to a Biotage solvent reservoir, mixed thoroughly and then eluted through the column. Column run-off was collected in 20 L jerry cans.  $\mathbb{Z}$
- **b.** Ethyl acetate (25 **kg)** and Petroleum ether **(26 kg)** were charged to the **50** L reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans. <sup>2</sup>
- c. Ethyl acetate **(31 kg)** and Petroleum ether (22 **kg)** were charged to the **50** L reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 5 L glass lab bottles. <sup>2</sup>
- **d.** Ethyl acetate **(16 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run-off was collected in 20 L jerry cans.  $\mathbb D$
- e. The column was repeated as above with the remaining two portions of dry load silica prepared. M

**[0099]** The column fractions were sampled for product purity **(TLC [10 %** acetone in toluene, Rf **0.5]** to identify fractions with product. The accepted column fractions were combined and in a **100** L Bichi bowl. Toluene was used to rinse any crystalline material from accepted fraction vessels into the bowl. Evaporation was run under vacuum using a water bath temperature of 40 ± 10°C until no more solvent distilled. Toluene (1.7 kg) was charged to the bowl and to contents rotated until the solids dissolved. t-Butyl methyl ether (4.4 **kg)** was charged to the bowl over 20-40 min. The bowl contents were rotated for 12-24 h at a temperature of 20  $\pm$  5°C. The bowl contents were transferred to a 6 L Nutsche filter and the solvent removed **by** vacuum filtration. t-Butyl methyl ether **(620 g)** was charged to the bowl, transferred to the Nutsche filter and passed through the filter cake. The filter cake was air dried in the filter then transferred to a vacuum oven and dried at a setting of **30°C**  under vacuum to remove residual solvent. The solid was sampled for analytical and retention. The solid was transferred to screw-top Nalgene containers and stored at ≤-15 °C. Expected Yield: **1.68 -** 1.94 **kg** compound **9 (65-75 %).** 

# Synthesis of Compound **10**

**[0100]** Reagents were prepared as follows: N-Iodosuccinimide (241 **g,** 2.20 eq.) was dried in a vacuum oven with a setting of **30°C** under vacuum for 24 h. **A** solution of sodium chloride **(300 g)** in water **(3000 g)** was prepared in a **5** L lab bottle. **A** solution of sodium thiosulfate **(1100 g)** in water **(6000 g)** was prepared in a **50** L reactor and distributed into two portions.

**[0101]** Compound **8 (355 g,** 0.486 mol) and Compound **9** (634 **g, 1.10** eq.) were charged to a 20 L Bichi bowl followed **by** toluene **(1500 g)** and heated at 40 **±5C** until dissolved. Evaporation was run under vacuum using a water bath temperature of 35 ± 10°C until no more solvent distilled. Toluene **(1500 g)** was charged to the Bichi bowl. Evaporation was run under vacuum using a water bath temperature of 35 ± 10<sup>o</sup>C until no more solvent distilled. Dry dichloromethane (4000 **g)** was charged to the Bichi bowl. The bowl was rotated until the solids dissolved and the solution was transferred to a 5L reactor with a jacket temperature of **20°C ±5C.** Dry dichloromethane **(710 g)** was charged to the Bichi bowl. The bowl was rotated to rinse the bowl surface and the solution was transferred to the **5** L reactor. The reactor contents were sampled for reagent ratio **IPC** (H1 NMR). Dried **<sup>N</sup>** lodosuccinimide was charged to the reactor under a nitrogen atmosphere and the reactor was stirred for 5-15 min. The reactor contents were adjusted to 20°C ± 3°C. Trimethylsilyl trifluoromethanesulfonate (5.94 **g, 0.055** eq.) in dry **DCM (60 g)** was charged to the reactor over 5-15 min. maintaining the contents temperature at 20°C ± 3°C. The reaction mixture was stirred at 20°C ± 3°C for 20 ± 3 min. The reactor contents were sampled for reaction completion (HPLC). N-Methylmorpholine **(98 g,** 2 equiv.) was charged to the reactor and mixed thoroughly. One of the portions of the sodium thiosulfate solution prepared above was charged to the **50** L reactor. The 5L reactor contents were transferred to the SOL reactor containing the sodium thiosulfate solution and mixed thoroughly. The bottom layer was discharged to a HDPE jerry can.

**[0102] DCM (570 g)** was charged to the **5** L reactor with the top layer from the SOL reactor and mixed thoroughly. The bottom layer was combined with the previous bottom layer in the HDPE jerry can. The top layer was transferred to a separate HDPE jerry can and retained until yield was confirmed. The combined organic phase (bottom layers) were charged to the **50** L reactor followed **by** another portion of sodium thiosulfate and mixed thoroughly. The bottom layer was discharged to a HDPE jerry can. The top layer was

retained in a HDPE jerry can until yield was confirmed. The sodium chloride solution was charged to the 50L reactor along with the organic phase (bottom layers) and mixed thoroughly. Silica gel **(1300g)** was charged to a Bichi bowl and fitted with a rotary evaporator. The bottom layer in the reactor was charged to the Bichi bowl. The bowl contents were rotated to prevent adsorption onto the bowl and evaporated under vacuum using a water bath temperature of 40 ± 5<sup>o</sup>C until no more solids distilled. The bowl contents were divided into two equal portions. Silica gel **(200g)** was charged to the Bichi bowl followed **by** dichloromethane **(700 g).** The bowl contents were rotated to ensure solids did not adhere to the bowl surface. The bowl was evaporated under vacuum at a water bath temperature of 40°C ± 10°C until no more solvent distilled. The bowl contents were divided into two portions and a portion was added to each of the previous silica gel samples.

**[0103]** Each portion was purified independently on silica gel using the following procedure (samples were stored at 15°C while awaiting purification): **A 150** L KP-SIL cartridge was installed in the Biotage system. Ethyl acetate **(15.5 kg)** and petroleum ether **(16.5 kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to two Biotage solvent reservoirs. The solvent reservoirs contents were eluted through the column so as to condition the column. The eluent was collected in 20 L jerry cans and discarded. **A**  portion of the dry load silica from above was charged to the Biotage Sample-Injection Module **(SIM)** and then eluted with the ethyl acetate/petroleum ether as follows:

- a. Ethyl acetate **(6.2 kg)** and Petroleum ether **(6.6 kg)** were charged to a 50L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir. Column run-off was collected in 20 L jerry cans.  $[2]$
- **b.** Ethyl acetate **(19.5 kg)** and Petroleum ether **(19.2 kg)** were charged to the **50** L reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans. <sup>2</sup>
- c. Ethyl acetate **(13.6 kg)** and Petroleum ether **(12.3 kg)** were charged to the **50** L reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans. <sup>2</sup>
- **d.** Ethyl acetate (14.2 **kg)** and Petroleum ether **(11.9 kg)** were charged to the **50** L reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans. <sup>2</sup>

e. Ethyl acetate **(29.7 kg)** and Petroleum ether **(22.9 kg)** was charged to a Biotage solvent

reservoir and then eluted through the column. Column run-off was collected in 20 L ierry cans up to fraction 11 and then 5L HDPE jerry cans. 2

- **f.** Ethyl acetate **(15.5 kg)** and Petroleum ether **(11.0 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run-off was collected in 5L HDPE jerry cans. 2
- **g.** Ethyl acetate **(29.7 kg)** and Petroleum ether **(13.2 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run-off was collected in 5L HDPE jerry cans. 2
- h. Ethyl acetate **(15.5 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run-off was collected in 5L HDPE jerry cans. *M*

**[0104]** Column fractions were sampled for product purity **(TLC** to identify fractions with product). Fractions that were **75 - 95 %** area compound **10** from the first two columns were combined in a Bichi bowl charged with silica gel (400 **g)** and evaporation was run under vacuum using a water bath temperature of 40  $\pm$  10<sup>o</sup>C until no more solvent distilled. The contents of the bowl were purified as follows: **A 150** L KP-SIL cartridge was installed in the Biotage system. Ethyl acetate **(15.5 kg)** and petroleum ether **(16.5 kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to two Biotage solvent reservoirs. The solvent reservoirs contents were eluted through the column so as to condition the column. The eluent was collected in 20 L jerry cans and discarded. The bowl contents were charged to the Biotage Sample-Injection Module **(SIM)** and then eluted with the ethyl acetate/petroleum ether as follows:

- a. Ethyl acetate **(6.2 kg)** and Petroleum ether **(6.6 kg)** were charged to a SOL reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir. Column run-off was collected in 20 L jerry cans.
- **b.** Ethyl acetate **(19.5 kg)** and Petroleum ether **(19.2 kg)** were charged to the **50**  L reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans.<sup>[2]</sup>
- **c.** Ethyl acetate **(13.6 kg)** and Petroleum ether **(12.3 kg)** were charged to the **50**  L reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans.
- **d.** Ethyl acetate (14.2 **kg)** and Petroleum ether **(11.9 kg)** were charged to the **50**

L reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans.

- e. Ethyl acetate **(29.7 kg)** and Petroleum ether **(22.9 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run off was collected in 20 L jerry cans up to fraction **11** and then 5L HDPE jerry cans. 2
- **f.** Ethyl acetate **(15.5 kg)** and Petroleum ether **(11.0 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run off was collected in  $5L$  HDPE jerry cans.  $\mathbb{Z}$
- **g.** Ethyl acetate **(29.7 kg)** and Petroleum ether **(13.2 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run off was collected in 5L HDPE jerry cans. 2
- h. Ethyl acetate **(15.5 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run-off was collected in 5L HDPE jerry cans.

**[0105]** The accepted column fractions from all three columns were combined in a Bichi bowl and evaporation was run under vacuum using a water bath with temperature of 40°C **±10°C** until no more solvent distilled. The contents of the bowl was sampled for analytical and retention. The bowl was sealed and transferred to storage at  $\leq -15$  °C. Expected Yield: 440 **-** 540 **kg** (52 **-** 64 **%** yield).

### Synthesis of Compound **11**

**[0106]** Dichloromethane was charged to a Bichi bowl containing compound **10 (635 g,**  0.345 mol) **(PN0699)** and heated at **30 ±10C** until dissolved. Methanol **(3.2 kg)** was charged to the bowl. The content of the bowl were adjusted to  $0 \pm 3$ °C. Acetyl chloride (54.1) *g,* 2 equiv.) in dichloromethane **(660 g)** was charged to the bowl maintaining the contents temperature at  $0 \pm 10^{\circ}$ C. The bowl contents were adjusted to  $20 \pm 3^{\circ}$ C and the mixture was stirred for 40-48 h. The bowl contents were sampled for reaction completion **IPC** (HPLC, pass). The bowl contents were adjusted to **0 ±3C.** N-methylmorpholine **(139 g,** 4 equiv.) was charged to the bowl and mixed thoroughly. The bowl contents were sampled for quench completion **IPC** (pH paper, pass ≤ pH7). The bowl contents were concentrated under vacuum with water bath at 35 ± 10°C. Ethyl acetate (4.8 kg) and water (5.5 kg) were charged to the Bichi bowl and rotated to dissolve the bowl contents. The bowl contents

were transferred to a 50L reactor and mixed thoroughly. The bottom layer was drained to a HDPE jerry can. The top layer was transferred to a Bichi bowl fitted with a rotary evaporator and the contents were concentrated under vacuum with a water bath at **35 10°C.** The bottom layer from the HDPE jerry can was charged to a 50L reactor with ethyl acetate **(1.5 kg)** and mixed thoroughly. The bottom layer was drained to a HDPE jerry can and held until yield was confirmed. The top layer was transferred to the Büchi bowl fitted with a rotary evaporator and the contents were concentrated under vacuum with a water bath at 35 ± 10°C. The contents of the bowl were sampled for analytical and retention. The bowl was sealed and transferred to storage at  $\leq -15$  °C. Expected Yield:  $518 - 633$  kg (90  $-$ **110 %** yield).

### Synthesis of Compound 12

**[0107]** Reagents were prepared as follows: Two portions of N-Iodosuccinimide (143 g, **3.90** eq.) were dried in a vacuum oven with a setting of **30°C** under vacuum for 24 h. **A**  solution of sodium chloride (450 **g)** in water **(1850 g)** was prepared in a **5** L lab bottle and distributed to 2 approximately equal portions. **A** solution of sodium thiosulfate **(230 g)** in water **(2080 g)** was prepared in a **5** L lab bottle and distributed to 4 approximately equal portions.

Compound **9** (504 **g, 1.30** eq.) was charged to a **50** L Bichi bowl containing compound **11 (607 g, 0.327** mol) followed **by** toluene **(1500 g)** and heated at 40 **±5C** until dissolved. Evaporation was run under vacuum using a water bath temperature of 35 ± 10<sup>o</sup>C until no more solvent distilled. Toluene **(1500 g)** was charged to the Bichi bowl. Evaporation was run under vacuum using a water bath temperature of  $35 \pm 10^{\circ}$ C until no more solvent distilled. Dry **DCM** (2400 **g)** was charged to the Bichi bowl. The bowl was rotated until the solids dissolved and half the solution transferred to the 5L reactor with a jacket temperature of **20°C ±5C.** The second half of the solution was transferred to a **5** L lab bottle. Dry DCM (710 g) was charged to the Büchi bowl. The bowl was rotated to rinse the bowl surface and half the solution was transferred to the **5** L reactor. The other half was charged to the **5** L lab bottle above and stored under nitrogen for use in the second batch. **A**  portion of dried N-Iodosuccinimide was charged to the reactor under a nitrogen atmosphere. The reactor contents were adjusted to  $-40^{\circ}$ C ± 3<sup>o</sup>C. Trimethylsilyl trifluoromethanesulfonate **(9.09 g,** 0.25 effective equiv.) in dry dichloromethane **(90 g)** was charged to the reactor over **15** min. maintaining the contents temperature at -40°C **±5C.** 

The reaction mixture was stirred at  $-40^{\circ}$ C  $\pm$  3°C for 30  $\pm$  5 min. then adjusted to  $-30^{\circ}$ C  $\pm$ **3 0C** over and stirred for **150** min. The reactor contents were sampled for reaction completion. N-Methylmorpholine **(33.1** *g,* 2 effective eq.) was charged to the reactor and mixed thoroughly. One of the portions of the sodium thiosulfate solution prepared above was charged to the **5** L reactor and mixed thoroughly. The bottom layer was discharged to a **5** L lab bottle. **DCM** (400 **g)** was charged to the **5** L reactor and mixed thoroughly. The bottom layer was combined with the previous bottom layer in a 5L lab bottle. The combined organic phases were charged to the **5** L reactor followed **by** another portion of sodium thiosulfate and mixed thoroughly. The bottom layer was discharged to a **5** L lab bottle. **A** portion of sodium chloride solution from above was charged to the reactor followed **by** the content of the previous lab bottle. The bottom layer in the reactor was charged to the Büchi and evaporated under vacuum using a water bath temperature of 40  $\pm$ **10 0C** until no more solvent distilled. The reactor was cleaned and dried.

**[0108]** The second portion of compound **9** and compound **11** were charged to the reactor and treated identically to first batch. Following organic extraction of the second batch, the reaction mixtures were combined in the reactor. **A** portion of sodium chloride solution was charged to the reactor and mixed thoroughly. Silica gel **(1700 g)** was charged to a Bichi bowl and fitted to a rotavapor. The bottom layer in the reactor was charged to the Büchi and evaporated under vacuum using a water bath temperature of  $40 \pm 10^{\circ}$ C until no more solvent distilled. The bowl contents were divided into two portions purified independently on silica gel. **A 150** L KP-SIL cartridge was installed in the Biotage system (commercially available from Biotage, a division of Dyax Corporation, Charlottesville, Virginia, **USA).** Ethyl acetate **(7.7 kg)** and petroleum ether (22.0 **kg)** were charged to the **50**  L reactor, mixed thoroughly and then transferred to two Biotage solvent reservoirs. The solvent reservoirs contents were eluted through the column so as to condition the column. The eluent was collected in 20 L jerry cans and discarded. **A** portion of the dry load silica from above was charged to the Biotage Sample-Injection Module **(SIM)** and then eluted with the ethyl acetate/petroleum ether as follows:

- a. Ethyl acetate **(1.5 kg)** and Petroleum ether (4.4 **kg)** were charged to a HDPE jerry can, mixed thoroughly and then transferred to a Biotage solvent reservoir. Column run-off was collected in 20 L jerry cans. 2
- **b.** Ethyl acetate **(18.6 kg)** and Petroleum ether **(8.8 kg)** were charged to the **50** <sup>L</sup> reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then

eluted through the column. Column run-off was collected in 20 L jerry cans. **M** 

- **c.** Ethyl acetate **(19.2 kg)** and Petroleum ether (8.4 **kg)** were charged to the **50** <sup>L</sup> reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans. **M**
- **d.** Ethyl acetate **(29.7 kg)** and Petroleum ether **(11.9 kg)** were charged to the **50** <sup>L</sup> reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans. <sup>2</sup>
- e. Ethyl acetate **(15.5 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run-off was collected in **5** L glass lab bottles. **M**

**[0109]** Column fractions were sampled for product purity **(TLC** to identify fractions with product). Fractions that were **75 - 95 %** area compound 12 from the first two columns were combined in a Bichi bowl charged with silica gel (400 **g)** and evaporation was run under vacuum using a water bath temperature of 40 ± 10°C until no more solvent distilled. Ethyl acetate **(7.7 kg)** and petroleum ether (22.0 **kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to two Biotage solvent reservoirs. The solvent reservoirs contents were eluted through the column so as to condition the column. The eluent was collected in 20 L jerry cans and discarded. The dry load silica containing the impure product was charged to the Biotage Sample-Injection Module **(SIM)** and then eluted as detailed below:

- a. Ethyl acetate **(1.5 kg)** and Petroleum ether (4.4 **kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir. Column run-off was collected in 20 L jerry cans. 2
- **b.** Ethyl acetate **(19.2 kg)** and Petroleum ether (8.4 **kg)** were charged to the **50** <sup>L</sup> reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans. **M**
- **c.** Ethyl acetate **(18.6 kg)** and Petroleum ether **(8.8 kg)** were charged to the **50** <sup>L</sup> reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans. <sup>2</sup>
- **d.** Ethyl acetate **(29.7 kg)** and Petroleum ether **(11.9 kg)** were charged to the **50** <sup>L</sup> reactor, mixed thoroughly, transferred to two Biotage solvent reservoirs and then eluted through the column. Column run-off was collected in 20 L jerry cans. <sup>2</sup>
- e. Ethyl acetate **(15.5 kg)** was charged to a Biotage solvent reservoir and then eluted through the column. Column run-off was collected in 5 L glass lab bottles. <sup>[2]</sup>

**[0110]** Column fractions were sampled for product purity **(TLC** to identify fractions with product, HPLC pass criteria **95 %** compound 12 and no single impurity **>** 2.5 **%).** The accepted column fraction from all three columns were combined in a Büchi bowl and evaporation was run under vacuum using a water bath temperature of 40 **±10 C** until no more solvent distilled. The contents of the bowl was sampled for analytical and retention. Bowl was sealed and transferred to storage at  $\leq -15$  °C. Expected Yield:  $494 - 584$  kg  $(52 -$ 64 **%** yield).

#### Synthesis of Compound **13**

**[0111]** Glacial acetic acid **(7.5 kg)** and ethyl acetate **(6.5 kg)** were combined in a suitable container and labeled as **"GAA/EA** solution". Sodium bicarbonate **(0.5 kg)** was dissolved in RO water **(10 kg)** and labelled as **"5%** w/w sodium bicarbonate solution." Palladium on activated carbon **(100g,** specifically Johnson Matthey, Aliso Viejo, California, **USA,** Product No. A402028-10) and **GAA/EA** solution **(335 g)** was charged into a reaction vessel in that order. Compound 12 **(270 g)** was dissolved in **GAA/EA** solution (1840 **g)** and transferred to a SOL reaction vessel. The solution was purged of oxygen **by** pressurization with nitrogen to **10** bar and then released. This was repeated twice more. The reactor contents were pressurized under hydrogen to **10** bar and then released. The reaction mixture was hydrogenated at 20 bar **H2** for **1.5** days. The pressure was then released and the solution purged of hydrogen **by** pressurization with nitrogen to **10** bar and then release. This was repeated once. Reaction mixture was filtered through a pad of Celite **(300 g).** The celite cake was washed with **GAA/EA** solution (2 x **5.5 kg).** Filtrates were combined and evaporated under vacuum (bath temperature  $40 \pm 5^{\circ}$ C). The residue was co-evaporated with ethyl acetate **(2.3 kg)** in two portions. The expected weight of the crude product was **-316 g. A**  Biotage system was equipped with **150** M KP-SIL cartridge with a 5L Sample Injection Module **(SIM).** Ethyl acetate **(10.6 kg)** and glacial acetic acid (1.4 **kg)** were charged to the **50**  L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir. The contents of the solvent reservoir were eluted through the column so as to condition the column. The eluent was discarded. The crude product was dissolved in ethyl acetate (422 **g)**  and glacial acetic acid **(55 g).** The resulting solutions were charged to the **SIM** and passed onto the column. The reaction mixture was chromatographed as follows:

a. Ethyl acetate **(13.8 kg)** and glacial acetic acid **(1.8 kg)** were charged to the **50** <sup>L</sup> reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir.  $\mathbb D$ 

- **b.** The contents of the solvent reservoir were eluted through the **SIM** onto the column and the eluent was collected in a 20 L jerry can.  $\mathbb D$
- **c.** Ethyl acetate **(10.3 kg),** glacial acetic acid **(1.3 kg)** and methanol **(206 g)** were charged to the **50** L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir. 2
- **d.** The contents of the solvent reservoir were eluted through the column and the eluent was collected in a 5 L jerry cans. 2
- e. Ethyl acetate **(6.6 kg),** glacial acetic acid **(0.9 kg)** and methanol (340 **g)** were charged to the **50** L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir. M
- **f.** The contents of the solvent reservoir were eluted through the column and the eluent was collected in  $\sim$  2.5 L fractions in 5 L jerry cans.  $\mathbb{Z}$
- **g.** Ethyl acetate (31.4 **kg),** glacial acetic acid (4.1 **kg)** and methanol (3.4 **kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir. 2
- h. The contents of the solvent reservoir were eluted through the column and the eluent was collected in 5 L jerry cans. 2

**[0112]** Fractions containing compound **13** were combined and evaporated under vacuum (bath temperature 40 ± 5°C). Residue was dissolved in ethyl acetate (3.1 kg) and washed with **5%** w/w sodium bicarbonate solution **(9.3 kg),** ensuring the **pH** of the aqueous medium was  $\geq 8$ . The ethyl acetate phase was evaporated under vacuum (bath temperature 40 **±5C).** The contents of the bowl was sampled for analytical and retention. Expected Yield: **182 - 207 g (71 - 81%).** 

# Synthesis of Compound **16**

**[0113]** Dry dichloromethane (2.5 **kg)** was charged to a Bichi bowl containing compound **13 (211 g, 76.5** mmol, **1.00** eq.) and rotated without heating until dissolved. **A** solution of (2,5-dioxopyrrolidin-1-yl) 4-acetylsulfanylbutanoate **(25.8 g,** 99.4 mmol, **1.30** equiv) in dry dichloromethane (200 **g)** was added to the Bichi bowl. The bowl was rotated for **1** hr at ambient temperature followed **by** concentration under vacuum with a water bath temperature of  $40 \pm 5$  °C. Toluene (0.8 kg) was added to the bowl and removed under vacuum with a water bath temperature of 40 ± 5°C twice. Toluene (0.8 kg) was added to the residue to dissolve. Silica gel **(557 g)** was loaded into the reaction vessel and solvents were removed under vacuum with a water bath temperature of 40 ± 5 °C. A Biotage system was

equipped with a **150** M KP- **SIL** cartridge with a 5L Sample Injection Module **(SIM).** Toluene **(10.1 kg)** and acetone **(1.0 kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir (Solvent **A).** The reaction mixture was purified as **follows:** 

- a. Solvent **A** was eluted through the column so as to condition the column. The eluent was discarded. M
- **b. Dry loaded silica gel was transferred to the SIM.**  $\Box$
- c. Toluene **(9.6 kg)** and acetone **(1.5 kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir (Solvent B). <sup>2</sup>
- **d.** Solvent B was eluted through the column and the eluent was collected in **5** L jerry cans. **M**
- e. Toluene **(53.6 kg)** and acetone (12.2 **kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to Biotage solvent reservoirs (Solvent C). <sup>2</sup>
- f. Solvent C was eluted through the column and the eluent is collected in 5 L jerry cans. **M**
- **g.** Toluene (8.4 **kg)** and acetone **(2.6 kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir (Solvent **D). M**
- h. Solvent **D** was eluted through the column and the eluent was collected in a **5** L jerry cans.  $\overline{?}$
- i. Toluene (23.4 **kg)** and acetone **(9.2 kg)** were charged to the **50** L reactor, mixed thoroughly and then transferred to a Biotage solvent reservoir (Solvent E). <sup>2</sup>
- **j.** Solvent **E** was eluted through the column and the eluent was collected in a **5** L jerry cans.  $\overline{2}$

Fractions containing compound **16** (pass criteria **90 %** compound **16** and no single impurity **>** 2.5 **%)** were combined and evaporated under vacuum (bath temperature 40 **5°C).** The residue was dissolved in tetrahydrofuran (4.4 **kg)** and concentrated under vacuum with a water bath temperature of 40  $\pm$  5 °C. The contents of the bowl were sampled for analytical and retention. Expected Yield: **169 - 192 g (76 - 86%).** 

#### Synthesis of Compound **17**

**[0114]** The reactor was marked at the 2.5L, **3.5L** and **3.9** L levels before starting and fit with a vacuum controller. Dichloromethane was charged to a Bichi Bowl containing 140 **g**  of compound **16** and transferred to the Reactor Ready vessel. Two rinses of **DCM (333 g)**  were used to transfer the contents of the Büchi bowl into the Reactor Ready vessel. Ethanol (2.50 **kg)** was added to the reactor ready. The reaction mixture was concentrated to the 2.5

L mark (target vacuum **250** mbar). Ethanol **(1.58 kg)** was added to the reactor ready and concentrated to the **3.5** L mark. The reaction was diluted to the **3.9** L mark with ethanol. Reactor contents were placed under inert gas **by** applying a partial vacuum and releasing with nitrogen. **A** slow flow of nitrogen was maintained during the reaction. Hydrazine monohydrate **(1.13 kg,** *1.11* L) was charged to the 5L Reactor Ready vessel under a nitrogen atmosphere. The temperature ramp was set to: initial temp **20°C,** final temp **60°C,**  with a linear temperature ramp over **50** min **(0.8** deg/min) and active control on the contents of the reactor. The vessel temperature was held at **60 °C** for 45 min. The cooling ramp temperature was set to: -2 deg/min, with the final temp 20 **°C.** The contents were discharged to suitable HDPE jugs and weights determined. Equal amounts were transferred to **8** polypropylene centrifuge containers with FEP encapsulated seals. Each centrifuge container was charged with ethanol **(750 g)** and agitated for **30** min at ambient. The containers were centrifuged **(5300** RCF, **15°C, 30** min). Residual hydrazine on the outside of the containers was removed **by** rinsing the outside of the bottles with acetone then water before taking out of fume hood. The supernatant in the centrifuge containers was decanted and the residual pellet was dissolved in Low Endotoxin water **(LE** water) **(1960 g)** and transferred to a **5** L Reactor Ready vessel. The contents were agitated at medium speed while bubbling air through the solution using a dispersion tube approximately 15-20 min for every **1.5** hrs. The reaction was then stirred overnight at 20 **°C** in a closed vessel. Once **IPC** indicated free pentamer composition was below **3%** (area **%** of the total reported) the reaction was considered complete. Filtration (using a P3 sintered glass funnel and **5** <sup>L</sup> Buchner flask) was required if there were any insoluble material present in reaction mixture. Contents of the reactor were freeze-dried in 2 Lyoguard trays. The shelf temperature was set at **-0.5 °C** for **16-20** h and then at 20 **°C** until dry. Freeze- dried product was dissolved in **LE** water (840 **g)** and divide equally between **6** centrifuge bottles. Acetone **(630 g)** was added to each container agitated for **15** minutes. Isopropanol **(630 g**  per container) was added to each container and agitation continued for 20 min. Contents were centrifuged at **5300** RCF at **15°C,** for **1** h. The supernatants were discarded and each pellet was dissolved in water **by** adding **LE** water (140 **g)** to each container and then agitating the mixture at ambient using an orbital shaker until the pellets dissolved. Acetone **(630 g)** was added to each container and agitated for **15** minutes. Isopropanol **(630 g** per container) was added to each container and agitation continued for 20 min. The contents were centrifuged at **5300** RCF at **15°C,** for **1** h. The supernatants were discarded and each

pellet was dissolved in water **by** adding **LE** water **(100 g)** followed **by** agitation at ambient. The solutions were transferred to a Lyoguard tray and bottles were rinsed with more **LE**  water **(66 g** each) and the rinses were transferred to the same tray. The product was freeze dried **by** setting the shelf temperature at **-0.5 °C** for **16-20** h and then at 20 **°C** until dry. Freeze-dried product was sampled for analytical and retention. The Lyoguard Tray was double-bagged, labelled and stored in the freezer  $(s - 15 \degree C)$ . The potency of freeze-dried product was determined using qHNMR. This procedure afforded Crude Penta Dimer **17.**  Expected Yield: **26.1 - 35.5 g (61 - 83 %).** 

**[0115]** The identity of the compound **17** was determined **by** 1H and **<sup>1</sup> <sup>3</sup> <sup>C</sup>**NMR using a **500**  MHz instrument. A reference solution of t-butanol was prepared at 25 mg/mL in D<sub>2</sub>O. Samples were prepared at **13** mg/mL in **D20** and the reference solution is added to the sample. The composition of the final test sample was **10** mg/mL of the Penta Dimer and **5**  mg/mL of t-butanol. The <sup>1</sup>H and <sup>13</sup>C spectra were acquired and integrated. The resulting chemical shifts were assigned **by** comparison to theoretical shifts. The 1H NMR and **<sup>1</sup> <sup>3</sup> <sup>C</sup>**NMR spectra are shown in Figures **1** and 2 respectively.

### *Example 5 - Conversion of Crude Penta Dimer to Free Base Form.*

**[0116]** Amberlite **FPA91** (1.46 **kg;** 40 **g/g** of Crude Penta Dimer **-** corrected for potency) was charged to a large column. **A** solution of **8** L of **1.0** M NaOH was prepared **by** adding NaOH **(320 g)** to **LE** water **(8.00 kg)** in a **10** L Schott Bottle. This solution was passed through Amberlite resin over a period of **1** hour. **LE** water (40.0 **kg)** was passed through the Amberlite resin. The resin was flushed with additional LE water  $\left(\sim\!10\right)$  kg aliquots) until a **pH** of **< 8.0** was attained in the flow-through. The crude Penta Dimer (49 **g, PN0704),**  stored in a Lyoguard tray, was allowed to warm to ambient temperature. **LE** water (400 **g)**  was added to the Lyoguard tray containing Crude Penta Dimer (49 **g)** and allowed to fully dissolve before transferring to a **1** L Schott bottle. The tray was rinsed with a further charge of **LE** water (200 **g)** and these washings were added to the Schott bottle contents. The Crude Penta Dimer solution was carefully poured onto the top of the resin. The **1** L Schott bottle was rinsed with **LE** water (200 **g)** and loaded this onto the resin. The Amberlite tap was opened to allow the Crude Penta Dimer solution to move slowly into the resin over **~5**  min. The tap was stopped and material left on the resin for **-10** min. **LE** water was poured onto the top of the resin. The tap was opened and eluted with **LE** water, collecting approximately **16** fractions of **500** mL. Each fraction was analyzed **by TLC** charring **(10%** 

H2SO4 in EtOH). **All** carbohydrate containing fractions were combined and filtered through a Millipore filter using a  $0.2 \mu m$  nylon filter membrane. The solution was divided equally between **5 - 6** Lyoguard trays. The filtration vessel was rinsed with **LE** water **(100 g)** and divided between the trays. The material was freeze dried in the trays. The shelf temperature was set at **-10°C** for **16-20** hr and then at **+10 °C** until the material was dry. **LE**  water **(150 g)** was charged to all but one of the Lyoguard trays and transferred this into the one remaining tray containing dried material. Each of the empty trays was rinsed with a further charge of **LE** water **(100 g)** and this rinse volume was added to the final Lyoguard tray. The final Lyoguard tray was freeze dried. The shelf temperature was set at **- 10°C** for **16-20** hr and then at **+10°C** until the materials dry. The product was sampled for analytical and retention. Dried material was transferred to HDPE or PP containers and stored at  $\leq$  -**15°C.** Expected yield: **31 -** 34 **g (86 -** 94 **%).** 

**[0117] TCEP** reduction of the disulfide bond in the dimer is rapid and nearly stoichiometric. Use of a stoichiometric reduction with **TCEP** afforded approximately 2 equivalents of glucosamine pentasaccharide monomer. Specifically, the pentasaccharide dimer was dissolved in reaction buffer **(50** mM **HEPES** buffer **(pH 8.0))** containing **1** molar equivalent of **TCEP.** After **1** hour at ambient temperature, the reaction was analyzed **by**  HPLC with **CAD** detection. Under these conditions, conversion to the penta-glucosamine monomer (peak at **- 10** minutes) was nearly complete (penta glucsamine dimer peak at **11.5** minutes) **-** See Figure 4. The remaining unannotated peaks were derived from the sample matrix. Based on the balanced chemical equation, the added **TCEP** was largely converted to **TCEP** oxide and any residual **TCEP** inhibited air oxidation back to the dimer prior to addition to the conjugation reaction. For simplicity, glucosamine pentasaccharide can be added based on input dimer and assuming **>95%** conversion to the monomer under these conditions.

**[0118]** The identity of the Penta Dimer was determined **by** 1H and **<sup>1</sup> <sup>3</sup> <sup>C</sup>**NMR using a **500**  MHz instrument. A reference solution of t-butanol was prepared at 25 mg/mL in D<sub>2</sub>O. Samples were prepared at **13** mg/mL in **D20** and the reference solution was added to the sample. The composition of the final test sample was **10** mg/mL of the Penta Dimer and **5**  mg/mL of t-butanol. The 1H and **<sup>1</sup> 3C** spectra were acquired and integrated. The resulting chemical shifts are assigned **by** comparison to theoretical shifts. 1H and **<sup>1</sup> <sup>3</sup> <sup>C</sup>**NMR spectra are shown in Figures **1** and 2 respectively.

# **Example 5 - Conversion to the Penta Saccharide Monomer of Example 4 with the TT-***Linker*

# *of Example 2 to provide for a Vaccine ofthis invention (compound 18)*

**[0119]** The TT monomer-linker intermediate of Example 2 was reacted with increasing concentrations of 4 **- 70** pentameric glucosamine molar equivalents **(2-35** pentasaccharide dimer molar equivalents) for 4 hours at ambient temperature. The crude conjugates from each titration point were purified **by** partitioning through a **30** kDa MWCO membrane. Each purified conjugate sample was analyzed for protein content, payload density **by SEC-MALS**  and monomer **/** aggregate content **by SEC** HPLC. The data showed saturation of the payload density at **50** pentameric glucosamine equivalents. Based on the **SEC** HPLC analysis, the aggregate content increased as the pentasaccharide monomer charge was increased and appeared to reach steady state levels of an approximately 4 **%** increase starting at **30**  pentameric glucosamine equivalents. Based on these results, the pentasaccharide dimer charge selected for subsequent conjugation reactions was 25 molar equivalents, corresponding to a theoretical charge of **50** molar equivalents of pentameric glucosamine.

**[0120] A** series of three trial syntheses followed **by** a GMP synthesis of compound **18**  were prepared as per above. Each of the resulting products was evaluated for potency **(by ELISA** assay) and payload density (molar ratio of pentameric glucosamine to tetanus toxoid).





These results evidence very high loading factors for the compounds of this invention.

**[0122]** The foregoing description has been set forth merely to illustrate the invention and is not meant to be limiting. Since modifications of the described embodiments incorporating the spirit and the substance of the invention may occur to persons skilled in the art, the invention should be construed broadly to include all variations within the scope of the claims and equivalents thereof.

### WHAT **IS** CLAIMED **IS:**

1. **A** compound represented **by** formula I:

(A-B)x-C **<sup>I</sup>**

where A comprises from 3 to 12 repeating  $\beta$ - $(1\rightarrow 6)$ -glucosamine units or mixtures thereof having the formula:



B is of the formula:



where the left side of the formula is attached to **C** and the right side is attached to **A;**  and **C** is tetanus toxoid having at least **31** reactive amino functionalities;

*x* is an integer from about **31** to about **39;** 

*y* is an integer from **1** to **10;** and

R is hydrogen or acetyl provided that no more than 40% of the R groups are acetyl wherein said tetanus toxoid comprises at least **31** reactive amino groups and at least **90**  percent **by** number of the toxoid is in monomeric form.

2. **A** compound according to claim **1,** wherein **A** is:



$$
\overline{\text{or}}
$$



**3. A** compound represented **by** formula **11:** 

 $(A'-B)x-C$  **11** 

wherein **A'** is



B is of the formula:



where the left side of the formula is attached to **C** and the right side is attached to **A;**  and **C** is tetanus toxoid having at least **31** reactive amino functionalities;

*x* is an integer from about **31** to about **39;** 

*y* is an integer from **1** to **10;** and

R is hydrogen or acetyl provided that no more than 40% of the R groups are acetyl wherein said tetanus toxoid comprises at least **31** reactive amino groups and at least **85**  percent **by** number of the toxoid is in monomeric form.

4. The compound of any one of claims **1** to **3,** wherein the amount of non monomeric toxoid is less than about **5** weight percent.

**5.** The compound of any one of claims **1** to **3,** wherein the amount of non monomeric toxoid is less than about **0.5** weight percent.

**6. A** pharmaceutical composition comprising a pharmaceutically acceptable diluent and an effective amount of the compound of claim **1.** 

**7. A** pharmaceutical composition comprising a pharmaceutically acceptable diluent and an effective amount of the compound of claim 2 wherein said composition comprises no more than **3** weight percent of low molecular weight amino compounds.

**8. A** pharmaceutical composition comprising a pharmaceutically acceptable diluent and an effective amount of the compound of claim **3** wherein said composition comprises no more than **3** weight percent of low molecular weight amino compounds.

**9.** The pharmaceutical composition according to any one of claims **6-8,** wherein said composition comprises less than 2 weight percent of low molecular weight amino compounds.

**10.** The pharmaceutical composition according to claim **9,** wherein said composition comprises less than **1** weight percent of low molecular weight amino compounds.

**11. A** pharmaceutical composition according to claim 4, wherein the effective amount of the compound of claim **1** is an amount sufficient to kill microbes *in vivo,* when a patient has an effective white blood cell (WBC) count of at least about 2,000.

12. **A** pharmaceutical composition according to claim **5** wherein said compound is selected from the group consisting of:





FIG. 1

 $1/4$ 







 $2/4$ 



 $FIG. 3$ 



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